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Contribution of proteases and cellulases produced by solid-state fermentation to the improvement of corn ethanol production

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Abstract

By cultivating a strain of *Aspergillus tubingensis* on agro-industrial by-products using solid-state fermentation technology, a biocatalyst containing more than 130 different enzymes was obtained. The enzymatic complex was composed mainly of hydrolases, among which a protease, an aspergillopepsin, accounted for more than half of the total proteins. Cell-wall-degrading enzymes such as pectinases, cellulases and hemicellulases were also highly represented. Adding the biocatalyst to corn mash at 1 kg/T corn allowed to significantly improve ethanol production performances. The final ethanol concentration was increased by 6.8% and the kinetics was accelerated by 14 h. The aim of this study was to identify the enzymes implicated in the effect on corn ethanol production. By fractionating the biocatalyst, the particular effect of the major enzymes was investigated. Experiments revealed that, together, the protease and two cellulolytic enzymes (an endoglucanase and a β -glucosidase) were responsible for 80% of the overall effect of the biocatalyst. Nevertheless, the crude extract of the biocatalyst showed greater impact than the combination of up to seven purified enzymes, demonstrating the complementary enzymatic complex obtained by solid-state fermentation. This technology could, therefore, be a relevant natural alternative to the use of GMO-derived enzymes in the ethanol industry.

Keywords: Solid-state fermentation, Enzymes, Protease, Cellulases, Bioethanol, Corn, Purification, Characterization

Introduction

The use of solid-state fermentation technology to produce industrial enzymes is common in eastern countries such as India, China or Japan, and has been of growing interest for numerous applications worldwide over the past few decades (Bhargav et al. 2008; Brahmachari 2017; Subramaniyam and Vimala 2012). This technology can be used with a wide range of microorganisms, including fungi, yeasts and bacteria. It is particularly well suited to fungal species such as of *Aspergillus* and *Trichoderma*, to produce hydrolytic enzymes like amylases and cellulases, among others (Carboué et al. 2016; Singh et al. 2008; Pandey et al. 1999). Solid-state fermentation (SSF) has several advantages over submerged fermentation. From a

biotechnological point of view, it shows higher volumetric productivity, higher product stability, and lower catabolite repression (Hölker et al. 2004; Ashokkumar et al. 2001; Diaz-Godinez et al. 2001). Comparisons of metabolites resulting from solid-state or submerged fermentation attest that fungal metabolism is activated differently depending on the technology: Oda et al. (2006), for example, showed that secreted enzymatic complexes were of different composition according to whether the microorganism was cultivated under solid-state or submerged fermentation. With regards to environmental impact and economics, SSF is less water and time consuming, and it generates less waste. It is a relatively low-cost technology and it uses agro-industrial by-products or waste as substrate (Carboué et al. 2016; Panda et al. 2016).

The addition of enzymes is essential in the biochemical conversion of starchy and lignocellulosic biomass into fuel ethanol. Although starch-to-ethanol processes are already efficient, numerous recent works have evidenced

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that the use of accessory enzymes, besides amylases, could increase significantly ethanol yields and process efficiency in the corn ethanol industry (Klosowski et al. 2010; Mikulski et al. 2015). Especially, protease was shown to increase fermentation rate (Vidal et al. 2009) and ethanol yield by liberating free amino acids for the yeast (Perez-Carrillo et al. 2012; McAloon and Johnston 2014). Protease and possibly phytase have also shown positive impact on oil recovery in the corn dry-grind process (Luangthongkam et al. 2015). Cellulases and xylanases may also help in releasing starch bound to the corn fiber, and induce cost and energy savings by decreasing viscosity and reducing water binding to grains, thus facilitating centrifugation and drying steps (Harris et al. 2014).

A few research studies deal with producing several different enzymes with one microorganism by solid-state fermentation (Chutmanop et al. 2008; Mukhtar and Ikram-Ul-Haq 2009). The potential use of enzymatic complexes produced by SSF to lower the cost of enzymes in the ethanol process while valorizing by-products or residues such as distillers grains has also been reported (Hoskins and Lyons 2009; de Castro et al. 2011; Singhanian et al. 2015). However, little literature relates to the understanding of the applicative effect measured using enzymatic complexes obtained by SSF.

Previous works of strain and substrate screening and solid-state fermentation process optimization were carried out as part of the Osiris Program (data not published). It resulted in the development of a biocatalyst having a significant positive effect on corn ethanol fermentation process, for which a patent was filed (Guillaume et al. 2016). The aim of this work was to better understand the effect of this enzymatic product obtained by SSF on the production of ethanol from corn. Extensive characterization and fractionation of the biocatalyst were carried out to specify which enzymes were responsible for the overall effect measured.

Materials and methods

Biocatalyst production

The conditions of strain cultivation (temperature, humidity, air flow, stirring, kinetics) were previously studied and optimized to maximize enzyme concentration in the final product (data not published).

Microorganism

The microorganism used in this study to produce enzymes was the strain of *Aspergillus tubingensis* O27 from Soufflet's collection of microorganisms. The strain

was cultivated in potato dextrose agar (PDA) at 30 °C for 13 days prior to use, to obtain maximal viable spores.

Solid-state fermentation

A previous screening of several agricultural coproducts allowed to select a mix of rapeseed meal and wheat bran as a substrate, based on its textural, nutritional and enzyme inductor properties (data not published).

Fermentation medium contained 70% (w/w) rapeseed meal and 30% (w/w) wheat bran. The humidity of medium was adjusted with water to reach a final moisture level of 55%. Solid-state fermentation was carried out in a rotary-type automatic Koji-making equipment (Fujiwara Techno-Art Co., Ltd.) with 10 kg of initial dry matter of sterile fermentation medium. The medium was inoculated with 10^7 spores/g of initial dry matter and incubated at 33 °C for 51 h with a continuous ventilation of 35 Hz and discontinuous stirring. Water was added during culture to maintain the moisture level at $55\% \pm 2\%$. Solid-state fermentation was stopped by adding propionic acid.

Biocatalyst

At the end of SSF, the fermented medium was dried at 45 °C during 18 h to obtain a dry matter content of 90%. It was then ground with a Retsch Ultra Centrifugal Mill ZM300 using a 0.85-mm grid. The dry product, thus, obtained was called biocatalyst. It was stored at -20 °C. These conditions of post-treatment of the fermented medium were determined to preserve the product efficiency and enzymatic activities (data not shown).

Crude extract

For utilization in corn ethanol fermentation, a crude extract of the biocatalyst was prepared by adding water to the dry product (1/10 w/v), allowing for the soluble compounds to extract to the aqueous phase for 10–15 min at room temperature with moderate stirring (optimal time for maximum enzymatic activities in the extract). For proteomic analysis, the crude extract was centrifuged for 10 min at 3000 rpm at 20 °C to eliminate insoluble particles. The resulting extract contained 15 g/L of proteins.

Characterization of proteins and enzymes

Quantification of proteins

Protein concentrations were determined by DC protein Assay kit from Bio-Rad (Catalog Number 500-0116), according to the instruction manual.

Enzymatic assays

- β -Glucosidase (GLP) and cellobiohydrolase (cell-p) activities were estimated using, respectively, *p*-nitrophenyl β -D-glucopyranoside and *p*-nitrophenyl β -D-cellobioside (Sigma) as substrates. β -Glucosidase activity was inhibited by D-(+)-gluconic acid δ -lactone according to the procedure described by Gao et al. (2011). The assay mixture consisted of volume of substrate (0.58 mg/mL and 1.00 mg/mL, respectively) and half volume of enzymatic solution suitably diluted with acetate buffer 0.05 M pH 4.5. It was incubated at 30 °C and 40 °C (respectively) for 15 min. The reaction was stopped with 160 μ L of 1 M glycine pH 9.0 for GLP and 7.5% (w/v) sodium carbonate for cell-p. The *p*-nitrophenol liberated was measured at 405 nm and 420 nm, respectively. One unit of enzyme activity was defined as the amount of enzyme required to liberate 1 μ mol of *p*-nitrophenol (pNP) per minute under the standard assay conditions.
- To detect and quantify β -glucanase (AGL), xylanase (AXC) and cellulase (CMCell) activities, Azo-Barley glucan, Azo-Xylan of Birchwood and AZO-CM-cellulose (Megazyme) were, respectively, used as substrates. The enzymatic solutions diluted with acetate buffer at 0.1 M pH 4.6 (AGL and AXC) or 0.4 M pH 4.7 (CMCell) were incubated with the substrate at 30 °C or 40 °C for 10 or 20 min. The reaction was stopped with 3.0% (w/v) sodium acetate (CH₃COONa·3H₂O), 0.3% (w/v) zinc acetate and 70% (v/v) ethanol solution pH 5.0; 500 μ L of 96% (v/v) ethanol solution and 500 μ L 4.0% (w/v) sodium acetate (CH₃COONa·3H₂O), 0.4% (w/v) zinc acetate and 80% (v/v) ethanol solution pH 5.0, respectively, for AGL, AXC and CMCell activities. The optical density of the supernatant was measured at 590 nm. One unit is the amount of enzyme which, diluted at 1 U/mL and used under the conditions of the assay, results in the release of non-precipitable oligomers such as the optical density of the supernatant at 590 nm is 0.56; 0.93 and 1.0 for AGL, AXC and CMCell activities, respectively.
- Acid protease activity (PAC) was measured using casein solution (12% w/v) as substrate. The enzymatic solution diluted with lactate buffer 0.06 M pH 3.0 was incubated with the substrate at 40 °C for 2 h. The reaction was stopped with 10.0% w/v trichloroacetic acid. The optical density of the supernatant was measured at 275 nm. One unit is the amount of enzyme which, used under the conditions of the assay, results in the release of soluble peptides such

as the optical density of the supernatant is equal to a tyrosine solution at 120 μ g/mL.

- Polygalacturonase activity (PG) was determined by using the two cyanoacetamide method described by Gross (1982).

SDS-PAGE

SDS-PAGE was performed according to the protocol described by Laemmli (1970).

Identifications of proteins

Bottom-up proteomic analysis was carried out in nano-LC-MS/MS (nano-liquid chromatography tandem mass spectrometry) in triplicates.

Pretreatment of sample

Samples (100 μ g) were dissolved in 50 mM ammonium bicarbonate, pH 7.5. After reduction/alkylation (dithiothreitol at a final concentration of 10 mM, 2 h, 37 °C/iodoacetamide at final concentration of 50 mM, 30 min in the dark at room temperature), 2 μ g of trypsin (modified sequencing-grade trypsin, Roche) in 150 mM ammonium carbonate at pH 7.5, were added and proteins were incubated overnight at 37 °C while shaking. Then, the reaction was stopped with 10 μ L of 10% aqueous formic acid (v/v) and the peptides desalted on C18 stage tips micro desalting devices (ZipTip; Millipore Co.) according to the manufacturer's instructions.

LC-MS/MS

The system consisted of a RSLC Ultimate 3000 (RSLC nanosystem, Thermo Fisher Scientific) connected to a FT-ICR mass spectrometer (LTQ-FT Ultra, Thermo Fisher Scientific) using a nano-ESI source (TriVersa NanoMate, Advion Biosciences).

Six microlitre samples were injected after appropriate dilution on a capillary reversed-phase precolumn (C18 Acclaim PepMap100, 300- μ m i.d., 5-mm length, 5- μ m particle size; Thermo Scientific) before separation on a capillary reversed-phase analytical column (C18 Acclaim PepMap100, 75- μ m i.d., 50-cm length, 3- μ m particle size; Thermo Scientific), at a constant flow rate of 220 nL/min at 35 °C, with a gradient 2–40% buffer B in buffer A in 180 min (buffer A: water/acetonitrile/trifluoroacetic acid 98:2:0.1 (v/v/v), buffer B: water/acetonitrile/trifluoroacetic acid 10:90:0.1). Mass spectrometry was performed using the Top7 data-dependent acquisition method using the software Xcalibur 2.0.7 (Thermo Fisher Scientific): 1 full-scan FT MS at resolution 60,000; range of 470–2000 *m/z*, followed by seven LTQ MS/MS on the seven most intense peaks, with 90-s dynamic exclusion.

Protein identification

Proteome discoverer 2.2 (Thermo Fisher Scientific) was used to process the data and filter the results. All the data were submitted to Mascot search engine 2.6 (Matrix Science) against a concatenated sequence database built from the sequenced genomes of *Aspergillus niger* strains CBS513.88 and ATCC1015, *Triticum aestivum* and *Brassica napus* (all data from NCBI). The sequences from strains CBS513.88 and ATCC1015 were cured to eliminate redundancies. The following parameters were used: trypsin specificity, up to 2 miss cleavages; MS tolerance 10 ppm; MS/MS tolerance 0.5 Da, carbamidomethyl (Cys) as static modification, and oxidation (Met), deamidation (Asn, Gln), methylation (Asp, Arg, Lys), dimethylation/trimethylation (Arg, Lys) and methylation (Asp) as dynamic modifications. Results were further filtered out using False Discovery Rate (FDR) 0.01% threshold, minimum 2 peptides per protein and 2 ppm MS error tolerance. Label-free quantification was performed with Minora feature detection after retention-time alignment and feature detection. Intensity-based measurement was used from unique and razor peptides and was assigned to master proteins only.

Purification of enzymes

The optimized procedure for protein purification is shown in Fig. 3.

Protein fractionation by $(\text{NH}_4)_2\text{SO}_4$

Fractionation was obtained by cascaded additions of 40%, 55%, 65% and 100% of salt (based on saturation point). At each step, precipitation was carried out by stirring on ice for 30 min, and the solution was then centrifuged at $5000\times g$ for 15 min at 4 °C. The protein pellets were solubilized in a solution of 0.02 M histidine and 1.0 M ammonium sulfate pH 6.0 for further chromatography steps.

Chromatography

The system used for the purification of enzymes by chromatography was an Äkta purifier (GE Healthcare). For each method, collected fractions were analyzed for protein and enzymatic activities. The active fractions were pooled, assayed and stored at -20 °C.

Anion-exchange chromatography (IEXa)

Anion-exchange chromatography (IEXa) was carried out on a manually mounted column of 50 mL Sephadex Q FF gel (GE Healthcare). Chromatography was performed at 4 °C, at the flow rate of 10 mL/min. At the start, the column was in a solution of 0.02 M Histidine pH 6.0. After equilibration, the samples (200 mL) were loaded on the

column and 6-mL fractions were collected. Proteins were eluted using a solution of 0.02 M Histidine + 1 M chloride sodium pH 6.0 with a concentration gradient from 20 to 35%. Protein detection was monitored at 280 nm.

Hydrophobic-interaction chromatography (HIC)

HIC was performed on a 16:20 HP Hiprep phenyl HP column (GE Healthcare). Chromatography was performed at 20 °C with a flow rate of 3 mL/min. After equilibration with a solution of 0.02 M histidine and 1.0 M ammonium sulfate pH 6.0, the samples (20 mL) were loaded and 6 mL fractions were collected. Proteins were eluted using a solution of 0.02 M histidine pH 6.0 with concentration gradient from 0 to 100%.

Size-exclusion chromatography (SEC)

SEC was carried out with a Hiload Superdex column of 16-mm diameter and 600-mm length from GE Healthcare (120 mL of gel). The mobile phase was a solution of 0.1 M ammonium acetate pH 5.0, and the flow rate was 1 mL/min. Samples of 2 mL were injected.

Corn ethanol fermentation

Corn ethanol fermentation was carried out at laboratory scale under conditions reflecting the ones conducted in industrial corn fuel ethanol plants.

Corn mash

Corn grain was ground using a hammer mill (Electra) with a 0.8-mm grid. Mash was composed of 36% of corn ground, 10% of thin stillage and 56% of water. The slurry was first heated to 60 °C in a 4-L bioreactor stirred at 250–350 rpm. pH was adjusted to 5.5 with sulfuric acid. Liquefaction of starch was carried out by the addition of an alpha-amylase (Liquozyme SC DS, Novozymes) at 150 g per ton of corn and heating to 90 °C during 2 h. At the end of liquefaction, pH was adjusted to 5.3 with sulfuric acid. The mash was stored at -20 °C.

Microorganism

Dry active yeast *Saccharomyces cerevisiae* Ethanol Red® (Fermentis) was used for ethanol fermentation. Prior to use yeast was rehydrated in tryptone salt broth (1/10 w/v) at 35 °C for 30 min.

Ethanol fermentation

Simultaneous saccharification and fermentation was carried out at 32 °C during 51 h, in either flasks or bioreactors. The corn mash was inoculated with yeast to guarantee an initial concentration of 1.10^7 cell/mL. Urea was added at 1 g/L as nitrogen source.

Glucosylase (Spirizyme Excel XHS, Novozymes) was added at 420 g per ton of corn. Trials were done in duplicate. Flask model: trials were carried out in 250-mL baffled flasks containing 140 g of corn mash stirred at 120 rpm in an incubator. The anaerobic conditions were ensured by a rubber stopper and a needle (\varnothing 1.2 mm), allowing for the CO₂ to evacuate. Mass loss was used to follow ethanol production kinetics. Bioreactor model: trials were carried out in 2.5-L reactors (Biostat A+, Sartorius) containing 2 kg of corn mash. Stirring was performed at 350 rpm with Rushton blades. Gas meters (MilliGascounter[®]1, Ritter) allowed to measure CO₂ produced during fermentation (flow rate and total volume).

Addition of enzymatic products to corn mash fermentation

The biocatalyst or the purified fractions of it were added at the beginning of fermentation, along with the other ingredients. The biocatalyst was incorporated at 1 kg/T corn. Purified enzymatic fractions were incorporated at appropriate dosage to have equivalent enzymatic activity as added with the biocatalyst at 1 kg/T corn.

Analytical methods

Fermentation kinetics was followed either by mass loss (flask model) or CO₂ production measured by gas meter. During or at the end of fermentation, samples were collected for sugars (maltose and glucose), ethanol and glycerol analysis by HPLC. Samples were centrifuged at 3000 rpm for 15 min at 4 °C. Supernatants were appropriately diluted and filtered (25 mm GDX membrane nylon 0.20 μ m filter, Whatman) prior to analyses. High-performance liquid chromatography was performed with material from Waters (Isocratic E1515) using a Heater E1500 column. The effect of enzymatic products was calculated by comparison with CO₂, ethanol and glycerol produced in control conditions.

Calculation of ethanol yield

The yield of sugar conversion to ethanol was calculated as

$$\text{ethanol yield} \left(\frac{\text{g}}{\text{g}} \right) = \frac{\text{ethanol produced (g)}}{\text{initial glucose (g)}}$$

Initial glucose was determined by complete hydrolysis of corn mash by adding excess dosage of glucosylase (2.1 kg/T) during 16 h at 55 °C under agitation (190 rpm), followed by maltose and glucose analysis by HPLC. Total glucose was calculated as

$$\text{initial glucose (g)} = \text{maltose (g)} \times 1.1 + \text{glucose (g)}$$

Results and discussion

Enzymatic composition of the biocatalyst

The biocatalyst was produced by cultivating, under solid-state fermentation, a selected strain of *Aspergillus tubingensis* (O27) on a mix of wheat bran and rapeseed meal, as described in “Materials and methods”. The strain and blend of substrates were selected based on previous experiments (not shown).

The enzymatic composition of the biocatalyst was characterized. Mass spectrometry analysis of the crude extract allowed to identify 131 proteins, mainly hydrolases. A single protease (aspergillopepsin) accounted for more than half (58.0%) of the total proteins. Among the 20 most abundant enzymes, cell-wall-degrading enzymes were highly represented: pectinases (polygalacturonase, 3.9%; arabinofuranosidase, 2.3%), cellulases (cellobiohydrolases, 1.4%; endoglucanases, 1.3%; β -glucosidase, 1.0%) and hemicellulases (β -xylanases, 4.0%; β -xylosidase, 1.9%; β -galactosidases, 1.07%; endo-1,3- β -glucanase, 0.8%). Other enzymes such as amylases were also identified. Overall, the 20 most abundant enzymes represented almost 83% of the enzymatic complex (Fig. 1). Enzymatic assays confirmed that the crude extract contained high levels of protease, pectinase, cellulase and xylanase activity (Table 1).

The enzymatic complexes composition varies greatly with the fungal species, the strain and especially with the growth substrate, as evidenced by Ortiz et al. (2016) or De Vries et al. (2017) for genus *Aspergillus*. In the SSF technology, substrates have great impact on the quality and quantity of excreted enzymatic complexes. Wheat bran is a fiber-rich material well known to greatly induce enzyme production by SSF, more specifically cellulose- and xylans-degrading enzymes (Kang et al. 2004; Bansal et al. 2012; de Vries et al. 2017). Protease production can be induced by protein-rich agro-industrial residues such as cottonseed meal, soybean meal as well as wheat bran (de Castro and Sato 2014; de Castro et al. 2014). This is consistent with obtaining a protease- and cellulases/hemicellulases-rich enzymatic product by fermenting a strain of *Aspergillus* on a blend of wheat bran and rapeseed meal.

Effect of the biocatalyst on corn ethanol fermentation

The crude extract of the biocatalyst was assessed for its effect on ethanol production from corn mash at laboratory scale (conditions based upon industrial data, see “Materials and methods”).

The biocatalyst showed a significant positive effect on ethanol production kinetics and yield. Preliminary trials in flasks (data not shown) indicated that optimal effect was obtained with dosages of 0.5–1 kg/T corn. When the biocatalyst was added at 1 kg/T corn, CO₂ release

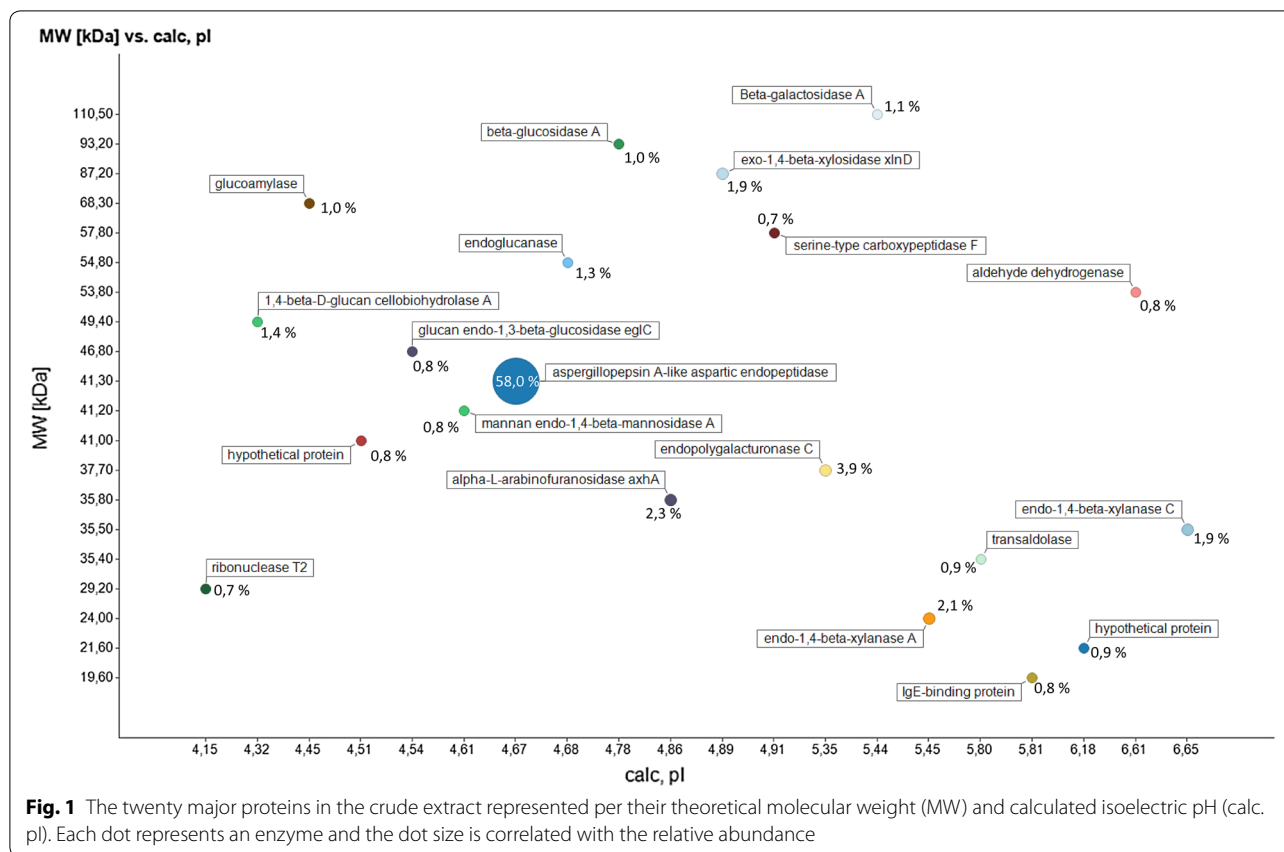


Table 1 Biocatalyst enzymatic profile

Enzymatic activity	Unit/g dry product
Protease (PAC)	115
β-Glucosidase (GLP)	11.8
Endo-xylanase (AXC)	208
Polygalacturonase (PG)	7022
β-Glucanase (AGL)	235
Cellulase (CMCell)	195

reached a maximum of 7.8 L/h at the end of yeast growth phase, increasing by 28% the highest value reached in control condition (Fig. 2). After 51 h of fermentation, total CO₂ produced was increased by 7% and glycerol was reduced by 17% with the addition of the biocatalyst. Kinetics was accelerated by more than 14 h. Ethanol concentration at 51 hrs reached 134.7 g/L, which represented an increase by 6.8% when the biocatalyst was added. Glucose-to-ethanol conversion yield of 45.0% was, thus, achieved (Table 2). Other trials carried out in flasks with several different industrial-like conditions indicated that

final yield increase with the use of the biocatalyst would rather be between 1.5 and 3.5% (data not shown). The difference in the ethanol increase may be explained by the fact that in this trial the fermentation reaction was not over after 51 h in the control condition (plateau not reached, Fig. 2).

These results are consistent with those obtained by Hoskins and Lyons (2009), who showed that a solid-state fermented product, obtained with a strain of *Aspergillus oryzae* cultivated on dried distillers' grains and solubles (DDGS), induced greater corn dextrin hydrolysis. Other studies demonstrated positive impacts of enzymatic products obtained by solid fermentation on fermentation processes. Zimbardi et al. (2013) have shown that an enzymatic product obtained by solid fermentation on wheat bran with a strain of *Colletotrichum graminicola*, contributed to the release of sugars from sugarcane broth, and thus increased the ethanol potential. Singhanian et al. (2015) have shown that a direct use of an enzymatic product (obtained by fermentation in a solid medium of wheat broth with a strain of *Penicillium janthinellum*) increased the hydrolysis of cellulose Avicel and steam pre-treated wheat straw used for ethanol production, thus contributing to yield improvement.

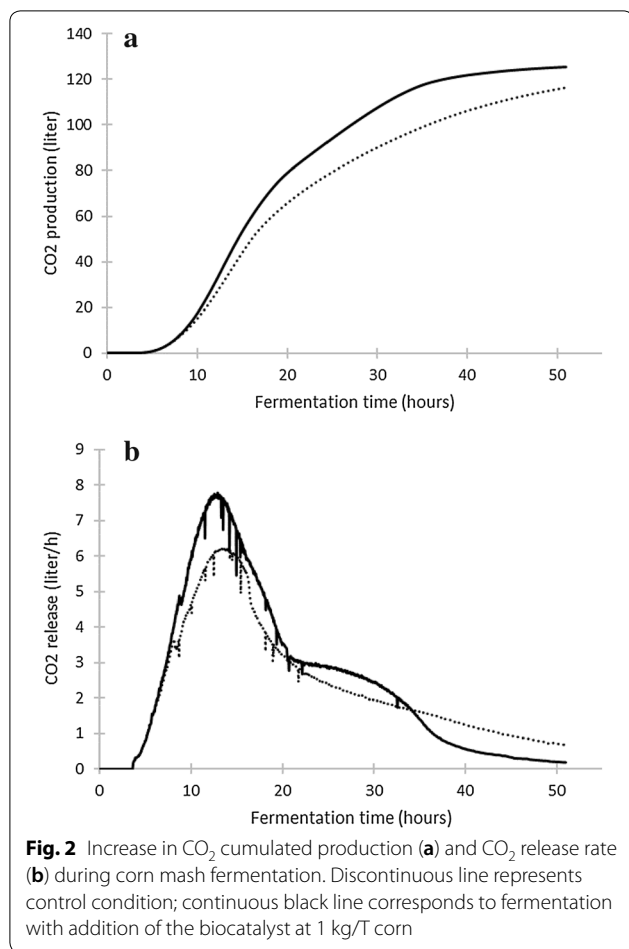


Table 2 Impact of the biocatalyst on the production of CO₂, ethanol and glycerol after 51 h of corn mash fermentation in bioreactor model

Final sample	Control	Biocatalyst 1 kg/T
CO ₂ (L/L mash)	58.28 ± 0.07	62.33 ± 0.31
Glycerol (g/L mash)	12.03 ± 0.01	10.04 ± 0.03
Ethanol (g/L mash)	126.15 ± 0.82	134.70 ± 0.22
Ethanol conversion yield (g/g initial glucose)	0.420 ± 0.002	0.450 ± 0.008

Data represent average ($n=2$) ± standard deviation

Proteolytic activity, which constitutes the main part of the enzymatic cocktail, may explain the effect of the biocatalyst measured on corn ethanol production. Indeed, protease may lead to an increase in FAN (free amino nitrogen) levels in the medium, as shown with corn and sorghum by Perez-Carrillo et al. (2012). The increase in FAN levels may also be consistent with less glycerol produced and higher ethanol yields (Albers et al. 1996). In terms of yeast metabolism, FAN is a direct usable source

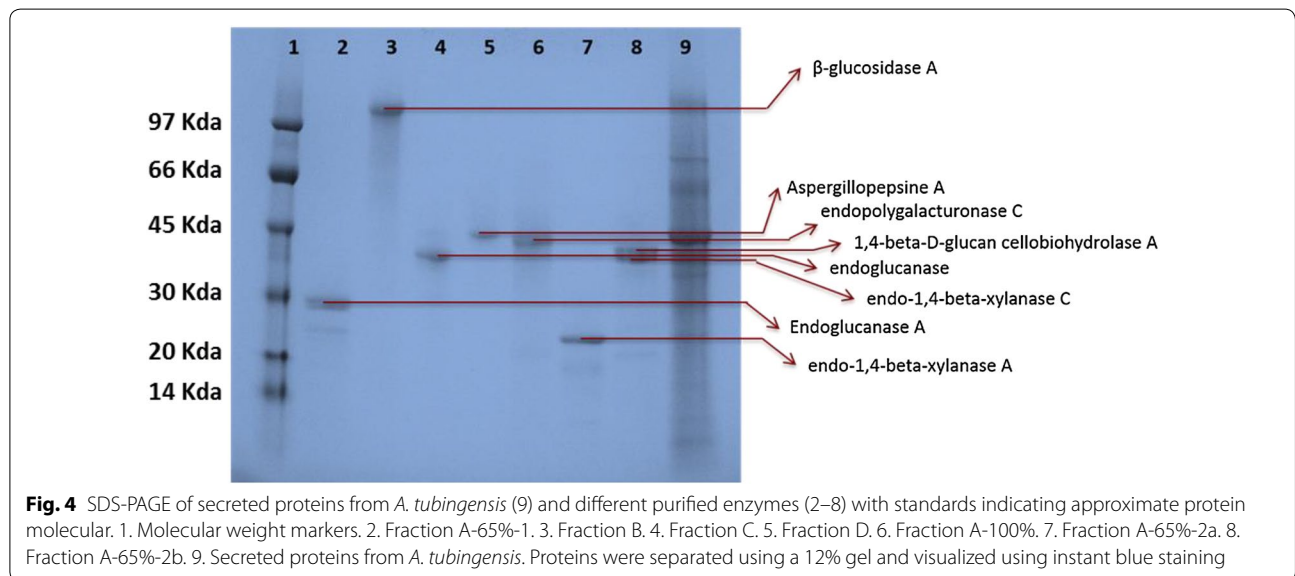
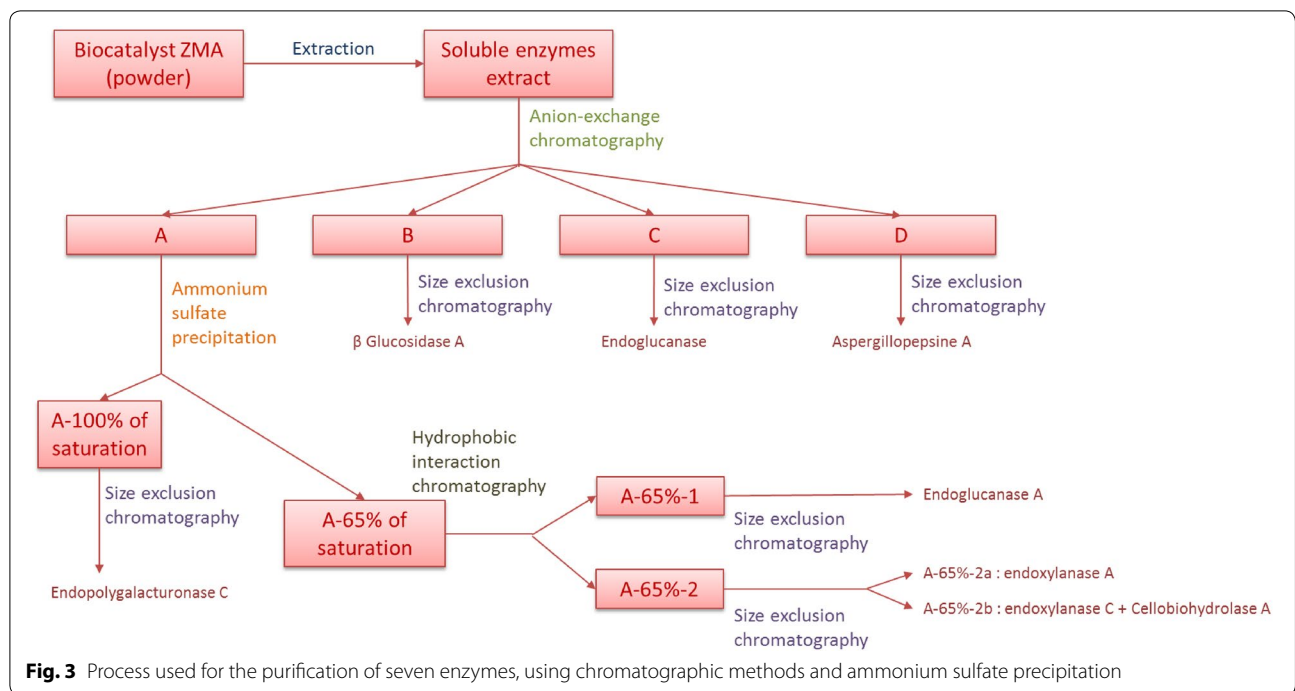
of amino acids for yeast protein synthesis, which suggests less need for using the tricarboxylic-acid circle. As this metabolic pathway is responsible for NADH production, less use may result in less glycerol production as a way to regenerate NAD⁺. As a consequence, the glucose catabolism pathway may be preferably oriented to generate energy for the yeast cell, through ethanol production (Rose and Harrison 1989).

Purification of the major proteins of the biocatalyst

To confirm and specify the part of protease and the other enzymes in the overall effect of the biocatalyst on corn ethanol production, the biocatalyst was fractionated. Seven enzymes among the most abundant were purified following a three-step purification methodology: capture, intermediate purification and polishing (Fig. 3). The fractions generated during enzyme purification were separated by one-dimensional SDS-PAGE Electrophoresis as shown in Fig. 4 and each fraction of purified enzymes was subjected to liquid digestion with trypsin prior to nano-LC-MS/MS analysis (data not shown). The fractions were shown to be practically pure, only one band per lane was observed except for the Fraction A-65%-2b, where the xylanase C band and the cellobiohydrolase A band (lane 8) were found. There was also a slight contamination of fraction A-65%-1 (lane 1) containing endoglucanase A by endo-1,4-beta-xylanase A. Specific activity was increased by 13-fold in the protease fraction (aspergillopepsin) and up to 250-fold in the β-glucosidase A fraction as shown in Table 3.

Proteomic analysis confirmed that the purified enzymes corresponded to seven of the most abundant enzymes having proteolytic and cell-wall-degrading activity, identified in the crude extract (data not shown), except for the endoglucanase A (an enzyme having β-1,3-glucanase activity) which was not identified in the biocatalyst at first. A further analysis of mass spectrometry data showed that it was due to the strict validation criteria of protein identification used in the first place (3 unique peptides), and that two unique peptides of the endoglucanase A were sequenced in the initial extract (data not shown). Together, the enzymes purified from the biocatalyst contributed to almost 70% of the total proteins identified in the biocatalyst.

Only two enzymes could not be isolated from one another: endo-xylanase C and cellobiohydrolase A. Although their theoretical pI (isoelectric point) was very different (4.32 and 6.65) and the difference in their molecular weight was greater than between other purified enzymes (Fig. 1), anion-exchange, hydrophobic-interaction and size-exclusion chromatography steps did not allow to separate them. According to the theoretical



pI of endo-xylanase C, this enzyme would have had to interact with the anion-exchange medium under experimental conditions. It means the actual pI of endo-xylanase C would be < 5. The use of either a more resolving size-exclusion chromatography column, or other chromatographic methods such as cation-exchange chromatography or chromatofocusing, may allow to separate endoxylanase C from cellobiohydrolase A.

Effect of individual and combined enzymes purified from the biocatalyst on ethanol production

The fractions of purified protease, cellulases, xylanases and pectinase were assessed in lab-scale fermentation trials to characterize the effect of each enzyme fraction on corn ethanol production. Combinations were also made to identify synergistic effects. To compare their impact, enzymatic fractions were added to corn mash at same enzymatic levels as with the biocatalyst added

Table 3 Specific activity of enzymatic fractions and purification efficiency by compared to the crude extract

Sample	Enzymatic activity	Specific activity in purified fractions (U/mg)	Specific activity in biocatalyst crude extract (U/mg)	Fold purification
Fraction D	Protease	7.70	0.582	13
Fraction B	β -Glucosidase	14.3	0.057	251
Fraction A-65%-2a	Endo-xylanase	42.8	0.596	72
Fraction A-65%-2b	Endo-xylanase	69.2	0.596	116
Fraction A-100%	Polygalacturonase	1882	19.7	96
Fraction A-65%-1	β -Glucanase	187	0.781	239
Fraction C	Cellulase	39.4	0.628	63

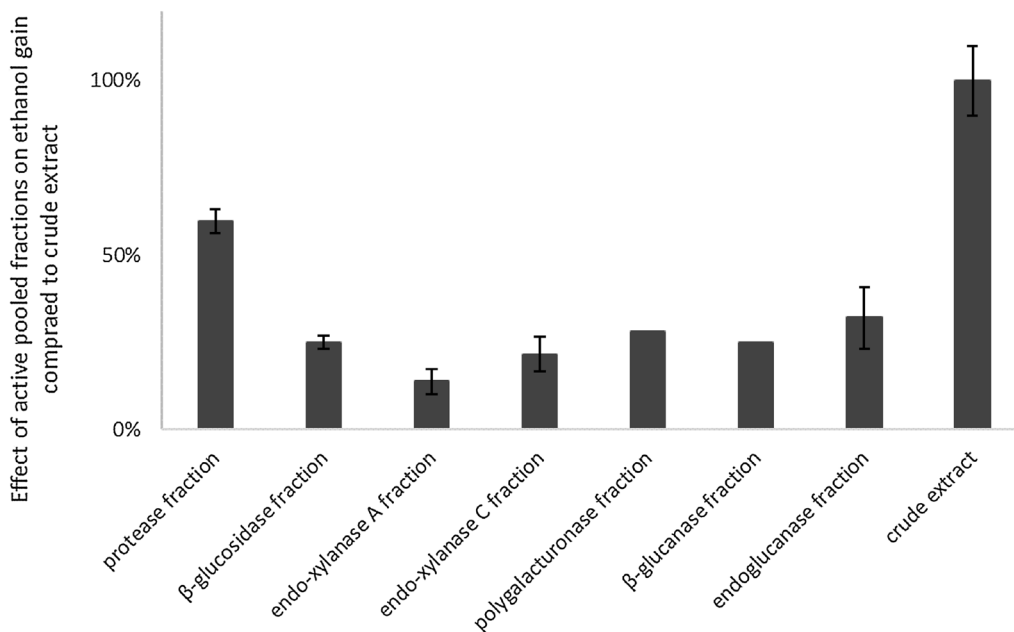
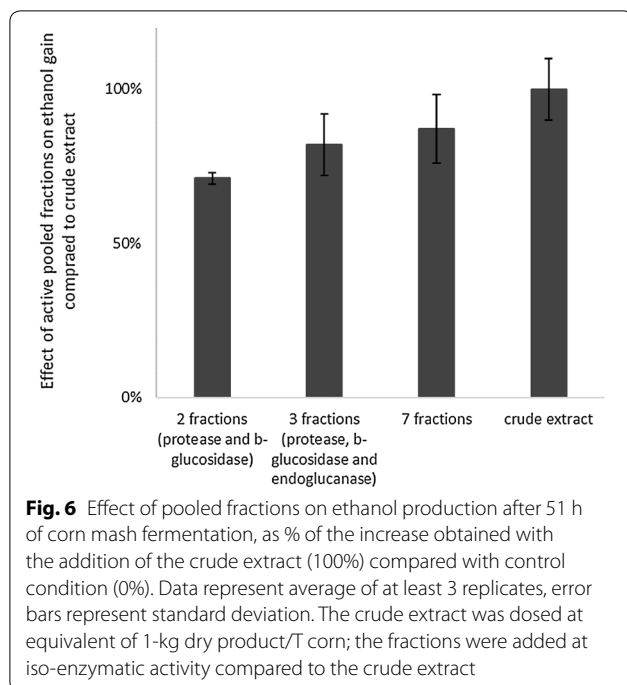


Fig. 5 Effect of each enzymatic purified fraction on ethanol production after 51 h of corn mash fermentation, as % of the increase obtained with the addition of the crude extract (100%) compared with control condition (0%). Error bars represent standard deviation ($n = 2$). The crude extract was added at equivalent of 1-kg dry product/T corn; the fractions were added at iso-enzymatic activity compared to the crude extract

at 1 kg/T. Interestingly, all seven fractions had a positive impact on ethanol production (Fig. 5). The protease was found to have the greatest impact among the enzymes and increased ethanol concentration by up to 60% of the overall effect of the crude extract. Levels of increase in final ethanol with the addition of protease were consistent with those of 2% obtained by McAloon and Johnston (2014) with the use of a commercial protease. The predominant part of proteolytic activity in the effect of the biocatalyst was, therefore, confirmed, although the crude extract kept a significant advantage over the single protease at same proteolytic activity level. As previously discussed, proteolytic activity induces FAN release which results in change in yeast metabolism and allow for more ethanol production.

Adding purified fractions of cellulases (endoglucanases or β -glucosidase) and xylanases into corn mash resulted in an increase in ethanol production of 0.3–0.6% after 51 h of fermentation, corresponding to 15–30% of the overall effect of the crude extract (Fig. 5). Such effect may be due to the hydrolysis of corn fibers, liberating reducing sugars to be fermented by the yeast, as shown by Zimbardi et al. (2013) with sugarcane, and by Idris et al. (2017) on sorghum stover. By adding cellulases obtained after solid-state fermentation of wheat bran by a strain of *Trichoderma reesei*, Yamane et al. (2002) also measured increases in alcohol production from sake mash. They showed that supplementation by a β -glucosidase had synergistic effect and further increased ethanol production, which our results tend to confirm.



Several pools of purified enzymatic fractions were formed to assess the combined effect of enzymes on ethanol production. The maximal effect was measured with the combination of all seven fractions (Fig. 6), indicating that each of these enzymes play a part in the overall effect of the biocatalyst. This combination allowed to reach 90% of the effect of the biocatalyst, while the enzymes accounted for approximately 70% of the total protein content. Our results indicate that the enzymes implicated in protein- and cell-wall degradation indeed have positive impact on ethanol production from corn as stated by literature.

Optimal combinations were found to be of protease together with cellulase (endoglucanase), and further associated with β -glucosidase. These combinations allowed to reach 70% and 80% of the overall effect of the crude extract, respectively. Yet, the additional two cellulolytic enzymes contribute to only 2% of the proteins in the biocatalyst. This result corroborate the significant positive effect of combined protease and cellulolytic enzymes on the performance of corn ethanol production, as shown by Kłosowski et al. (2010) and Mikulski et al. (2015). Luangthongkam et al. (2015) also reported the benefit provided by associating enzymes, showing greater performances with the combined use of proteases, phytases and cellulases.

Furthermore, the increase in ethanol yield measured with combinations of purified enzymes was found to be lower than the crude extract. This reveals the complexity in the biocatalyst applicative effect. It is likely that other cell-wall-degrading enzymes identified in the biocatalyst may be involved in the overall effect, such as arabinofuranosidase or mannosidase (Fig. 1).

Conclusion

This study demonstrated that our biocatalyst, obtained by solid-state fermentation, contained more than 130 enzymes. Thanks to the fractionation of the biocatalyst, the particular effect of seven major enzymes on corn ethanol production was elucidated.

Experiments with isolated and combined pure enzymes showed that, together, the protease and two cellulolytic enzymes (an endoglucanase and a β -glucosidase) were responsible for 80% of the overall effect of the biocatalyst. The crude extract of biocatalyst still showed higher performances than the combinations of 7 major enzymes, indicating the implication of minor enzymes, such as other cell-wall-degrading enzymes. Further fractionation works would then be necessary to totally explain the effect of the biocatalyst.

Abbreviations

AGL: β -glucanase activity; AXC: endo-xylanase activity; Cell-p: cellobiohydrolase activity; CMCCell: cellulase activity; GLP: β -glucosidase activity; PAC: protease activity; PDA: potato dextrose agar; PG: polygalacturonase activity; pI: isoelectric point; SSF: solid-state fermentation.

Authors' contributions

As project manager AG conducted the research, together with AT built the experimental design and performed scientific monitoring. AT performed and analyzed the corn ethanol trials. YC set up and performed the enzyme purification work. JV performed the nano-LC-MS/MS analyses and together with YC interpreted the data regarding protein identification. LL conducted the solid-state fermentation operations. All authors contributed to the discussion and the writing of the manuscript. All authors read and approved the final manuscript.

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Competing interests

The authors declare that they have no competing interests.

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The datasets used and/or analyzed during the current study are available from the corresponding author on reasonable request.

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