



Effect of thermal sludge processing on selected components of air quality in the vicinity of a wastewater treatment plant

Robert Cichowicz¹ · Artur Stelęgowski¹

Received: 17 April 2018 / Accepted: 9 November 2018 / Published online: 19 November 2018
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Abstract

Wastewater treatment plants (WWTPs) generate considerable amounts of sewage sludge. The thermal sludge treatment system (TSTS) is therefore one of the most important technological units of a WWTP. However, due to technological processes involved in thermal sludge treatment, specific chemical, physical and biological conditions may arise that can affect air quality both within the WWTP area and in its vicinity. This study uses data from experimental measurements taken in and around a WWTP to assess the impact of thermal sludge treatment on air quality. The selected facility is located in the Group Sewage Treatment Plant in the Lodz Agglomeration and serves a population of around one million. The concentrations of harmful gaseous substances, bacteria, fungi, particulate matter and thermal energy were investigated. The qualitative and quantitative characteristics of physical, chemical, and biological factors and their influence on air quality are presented.

Keywords Air quality · Particulate matter · Thermal energy · Bacteria and fungi

Introduction

Incineration processes are carried out in remotely controlled central and local heating systems. The use of fossil fuels and biomass can cause the emission of considerable amounts of harmful air pollutants into the environment (Cichowicz 2018; Cichowicz et al. 2017, 2016). However, municipal waste is a specific type of fuel, due to the presence of undesirable substances. Therefore, waste is incinerated in specially designed industrial systems. Thermal sludge treatment systems (TSTSs) have become an important element in large wastewater treatment plants (WWTPs). The increasing number of such systems in Poland and Europe is a testament to the high efficiency of TSTS (Pajak 2013).

The parameters of sewage sludge utilized in TSTS vary depending on the method of pre-treatment, which may be aerobic or anaerobic. Anaerobic digestion produces, among

others, biogas consisting of methane and carbon dioxide, while aerobic digestion produces carbon dioxide and ammonia (Arthurson 2008). Both aerobic and anaerobic digestion processes, biologically stabilize and reduce the volume of sludge, but also reduce the organic content and decreases its heating value by up to 50% (Fytli and Zabaniotou 2008). Decreasing the heating value is undesirable, since sewage sludge contains a significant amount of moisture, normally in the range of 72–98% (Bianchini et al. 2015), and requires thermal energy and dewatering for drying. Sewage sludge also contains significant amounts of nitrogen, heavy metals (Dai et al. 2007; Panepinto and Genon 2014), bacteria and other pathogens (Strauch 1991; Arthurson 2008). Neither aerobic nor anaerobic treatment provides sufficient sanitization (Arthurson 2008).

Thermal sludge treatment enables a large reduction in the volume of sewage sludge (by up to 90%), the destruction of organic compounds, the minimization of odors and the recovery of energy. However, the sludge delivered for incineration should first be dried. The drying process decreases the water content in sewage sludge, but also (depending on the drying temperature, residence time and other parameters) causes the release of amines, volatile organic and sulfur-containing compounds and odor (Ding et al. 2015). The incineration of sewage sludge results in the emission, inter alia, of heavy metals, dust, NO_x , SO_2 , HCl, and HF (Fytli

This work was presented at the 44th International Conference of Slovak Society of Chemical Engineering held in Tatraské Matliare on May 21–25, 2018.

✉ Robert Cichowicz
robert.cichowicz@p.lodz.pl

¹ Faculty of Architecture, Civil and Environmental Engineering, Lodz University of Technology, al. Politechniki 6, 90-924 Łódź, Poland

and Zabaniotou 2008). By applying the flue gas cleaning process, emission levels can be reduced by up to 50% for NO_x , over 95% for most heavy metals and by up to 99.9% for dust (Svoboda et al. 2016), depending on the dust filtration technology.

A specific system is required to reduce of the level of NO_x in flue gas. The two main systems available are based on Selective Non-Catalytic Reduction (SNCR) and Selective Catalytic Reduction (SCR). In the SNCR method, ammonia or urea is used at temperatures from 870 to 1260 °C. In the SCR method, ammonia is used in the presence of catalysts at temperatures from 260 to 540 °C (Shah et al. 1999). The incineration of wet sewage sludge, which contains a large amount of water (70–80% wt), results in very low emission of NO_x (Werther et al. 1995; Werther and Ogada 1999). However, ammonia emissions from anaerobically digested, pre-dried sewage sludge can be very high, up to 1.6 mg g^{-1} d.m. (Wielgosiński et al. 2016), depending on the combustion temperature. Special attention should also be paid to the efficiency of mercury removal in the dry flue gas cleaning process, which can attain 80–95% (Svoboda et al. 2016). However, due to the limitations of cleaning installations, some pollutants always penetrate into the environment.

The formation of problematic and hazardous chemical substances, bacteria and fungi during the storage, drying and incineration of sewage sludge can put people in danger and cause discomfort (Cichowicz and Stelęgowski 2018a, 2018b; Fytli and Zabaniotou 2008; Wielgosiński et al. 2016). Therefore, when planning the location of waste incineration plants, authorities should consider not only the technical and technological aspects but also the opinions of local communities. Public opinion is usually negative, due to widespread concerns relating to air quality and the amount of pollution in the vicinity of WWTP (Wielgosiński 2016).

The research literature on this topic mostly concerns the way WWTP personnel are affected by compounds such as dioxins (PCDD/F), polycyclic aromatic hydrocarbons (TCDD) and heavy metals (Cr, Cd, Ni, Pb), which form during the normal operation of municipal waste incineration systems (Carmen et al. 2003; Shih et al. 2006). Articles on existing TSTSs in WWTPs for the most part analyze the efficiency of air treatment processes and the concentrations of

pollutants in the exhaust gas (Pohorely et al. 2005; Panepinto and Genon 2014; Lu et al. 2013) or emissions from sludge drying (Ding et al. 2015). The objective of our study was to investigate the influence (significant, minor or none) of a TSTS on air quality in the near vicinity of a large WWTP (serving a population of around one million).

Experimental

The selected TSTS is located in the Group Sewage Treatment Plant of Lodz (GOŚ-ŁAM), in central Poland in Europe. The plant covers an area of approximately 41.3 ha and receives sewage in quantities of around 150–195 thousand m^3 day^{-1} . The sludge first undergoes an anaerobic procedure, producing biogas. After digestion (Table 1), most of the sludge is thermally treated (50–80%) and a small part is composted. The capacity of the TSTS is about 54 Mg d.m. day^{-1} (dry matter of sewage sludge). This amounts to around 18,000 Mg d.m. year^{-1} . The analyzed TSTS includes two independent technological lines (I and II), consisting of a storage subsystem, transportation and pre-drying of sludge. The elements of the TSTS include, among others, a fluidized-bed furnace, a recuperator of heat from exhaust gases, a steam boiler, a multi-cyclone, a bag filter, an exhaust fan, a chimney, and a steam distribution subsystem. In 2013, 2015, and 2016, between around 2 Mg and 10 Mg day^{-1} of the sludge was stored in the yard adjacent to the TSTS building.

After anaerobic treatment and mechanical dewatering, the sewage sludge is transported by screw conveyors to two 50 m^3 storage silos/tanks. Part of the sludge (around 20 m^3) was stored temporarily outside the TSTS building, in an adjacent area. The sludge is pumped to disc dryers inside the building, which pre-dry the material from around 20–24% to 30–32% dry matter. The energy for pre-drying, produced using saturated water vapor, is recovered from the incineration of sludge. Pre-dried sludge is thermally transformed (gasified) at a temperature of approximately 850 °C for at least 2 s. The sludge is gasified and incinerated in a fluidized bed furnace using “Pyrofluid” technology. For this purpose, two “Pyrofluid” fluidized bed furnaces by Veolia Water

Table 1 Composition of sewage sludge before drying (Wielgosiński et al. 2014)

Composition of sludge	Average value	Composition of sludge	Average value
pH/(–)	7.57	S/(% d.m.)	1.35
Dry matter/(%)	22.15	Cl/(% d.m.)	0.11
Moisture/(%)	79.37	Pb/(mg kg^{-1} d.m.)	57.06
Heating value/(MJ kg^{-1} d.m.)	10.84	Cr/(mg kg^{-1} d.m.)	207.55
Organic matter/(% d.m.)	59.45	Zn/(mg kg^{-1} d.m.)	1553.73
Total nitrogen/(% d.m.)	4.48	Hg/(mg kg^{-1} d.m.)	3.19
Ammonia nitrogen/(% d.m.)	0.70	Cu/(mg kg^{-1} d.m.)	413.49

Technologies are operated in the TSTS. Each of these furnaces is characterized by power of about 3.95 MW (“Pyrofluid” chamber, fluidized mixing, 4000–6000 m³ h⁻¹ regime, 750–800 °C sand bed temperature). The exhaust gases are cleaned by employing a dry method, using activated coal and sodium bicarbonate. Sodium bicarbonate is applied in doses to achieve a value below 40 mg Nm⁻³ for SO₂ and 9 mg Nm⁻³ for HCl in the flue gas. Since the incineration of anaerobically digested, pre-dried wet sewage sludge results in low emission of NO_x (Werther et al. 1995), no NO_x reduction system is applied. However, around 150–300 mg m⁻³ of activated carbon is injected to reduce the amount of mercury in the flue gas. Dedusting is performed in cyclones and filtration in bag filters. The dedusted and cleaned exhaust gases are directed into the atmosphere via two chimneys measuring 0.7 m in inner diameter and 25 m in height. The nominal temperature of the exhaust gases at the chimney outlet is 190 °C and the velocity is 14.16 m s⁻¹. The oxygen concentration in the flue gases is around 9%.

In this study, air quality was analyzed with respect to harmful factors such as the concentration of chemical substances (CO, CO₂, NO_x, SO₂, NH₃, CH₄, H₂S), physical factors (dust, thermal energy) and biological agents (bacteria and fungi). Data from automatic measurements of TSTS emissions were used to model the concentration of air pollutants in WWTP area of 108 ha. The data used in the analysis were collected during quarterly experimental measurements of air quality carried out in the years 2012–2015 at 7 points located in the area of the Group Sewage Treatment Plant WWTP itself, and at 8 points in its near vicinity (Procyk and Helbig 2013; Horodecka and Helbig 2014; SGS Eko-Projekt 2015; Skwarska and Horodecka 2016). An analysis was made of the interdependence between the concentration of air pollution in the vicinity of the TSTS (point number one in Fig. 1) and the “background” concentration in other locations. In 2016, additional measurements were performed for biological and physical factors within the TSTS building and in its close vicinity. The spread of pollution from the emitters was modeled using the OPA03 application (Eko-Soft). The model was implemented with a grid of 11,000 receptors. As will be discussed later, the model could not be validated due to the low concentration of pollution caused by the TSTS relative to the total air pollution in the vicinity of the WWTP.

Results and discussion

The highest annual concentrations in the exhaust gases from technological lines I and II were observed for SO₂, NO_x and NH₃ (Fig. 2). However, the average acceptable daily values for this type of system (according Directive 2010/75/EU) were exceeded on only four occasions, all of which were

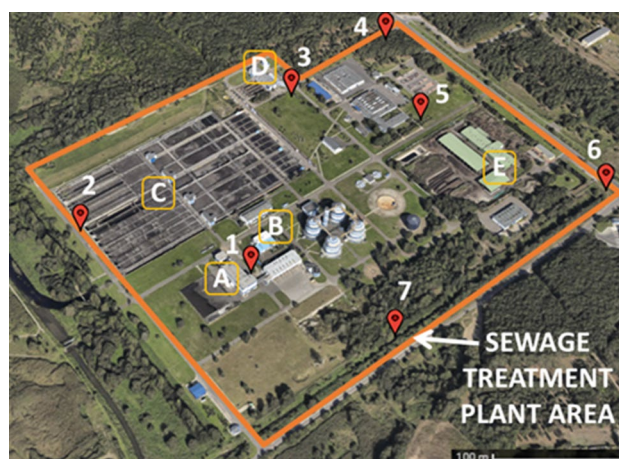


Fig. 1 Location of measurement points (1–7) in GOS–ŁAM, including the thermal sludge transformation system **a**, boiler and power plant **b**, sludge chamber **c**, inlet chamber and screen room **d** and the composting facility **e** Source: Google Maps

observed in 2012 and concerned SO₂. However, low emissions of NO_x and high emission of NH₃ were associated with the incineration of anaerobically digested (Wielgosiński et al. 2016), pre-dried wet/semi-dry sewage sludge (Werther et al. 1995; Werther and Ogada 1999).

Both technological lines underwent various periods of downtime during the period of analysis. These periods totalled on average 121 days a year for line “I” and around 74 days a year for line “II”. At the same time, no relationship was observed between the amounts of exhaust gases generated and the average daily temperature or wind speed (Fig. 3). Three basic phases were identified. In the first period, 9% of the year, no technological line was operational and no pollution was emitted. In the second period, 35% of the year, only one technological line was operational and the flow of exhaust gases was between 7000 and 11,000 Nm³ h⁻¹. In the third period, approximately 56% of the year, both technological lines were in operation and the flow of exhaust was approximately 15,000–20,000 Nm³ h⁻¹. As a consequence, the conditions associated with the emission of air pollution varied considerably.

Real average temperature conditions and the actual velocities of the exhaust gases were used in the model. The conditions for the first technological line were as follows: average temperature 172 °C, velocity 12.14 m s⁻¹. The average temperature was 167 °C for the second line and the velocity was 13.66 m s⁻¹. Only pollution associated with TSTS operation was analyzed using the model (Figs. 4, 5). The spatial distribution of air pollution connected to TSTS work showed that TST emission had a minor influence on air quality in the WWTP area. The share of the total concentration of pollution associated with TSTS emission did not exceed 0.30 µg m⁻³ for NO_x, 0.80 µg m⁻³ for SO₂,

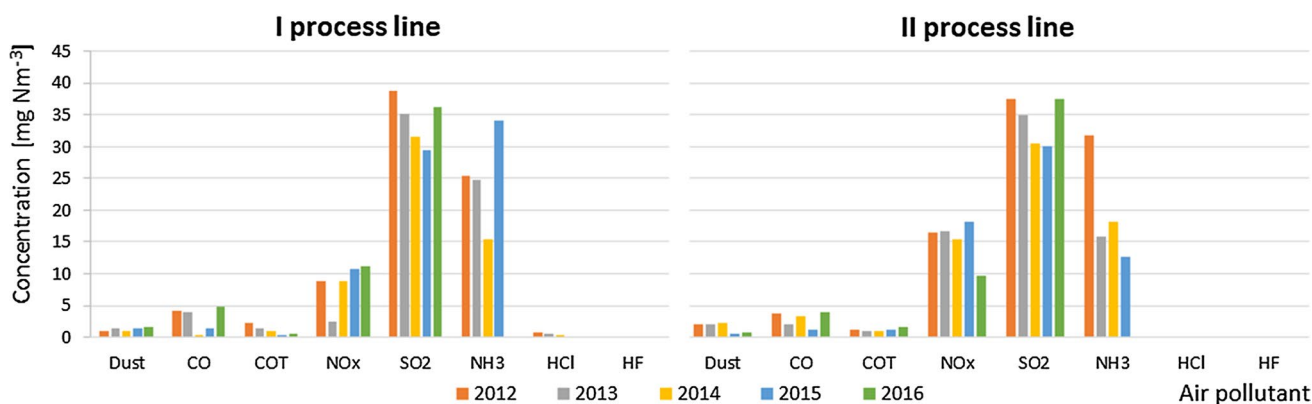


Fig. 2 Concentration of pollution in cleaned exhaust gases from technological lines I and II in 2012–2015 (11% O₂ concentration in flue gas volume)

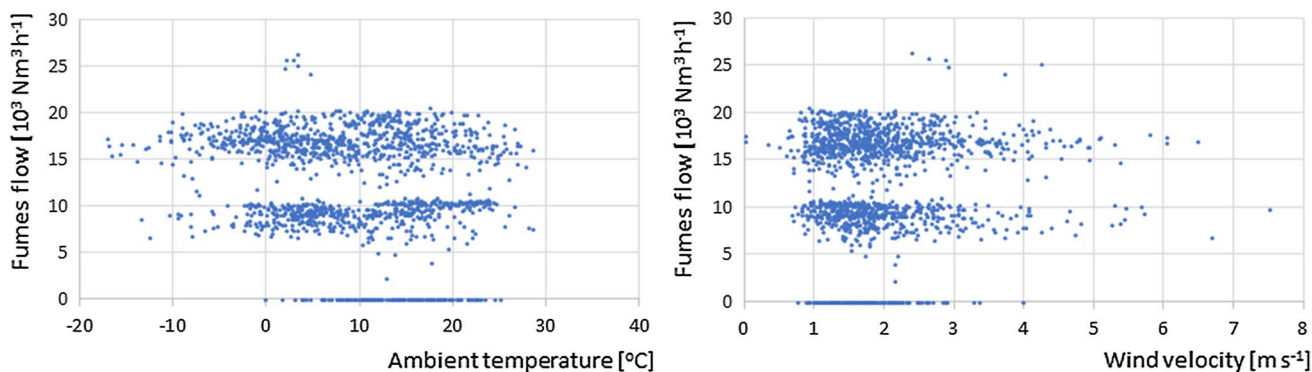


Fig. 3 Total flow of exhaust gases (lines “I” and “II”) depending on average daily temperature and wind speed

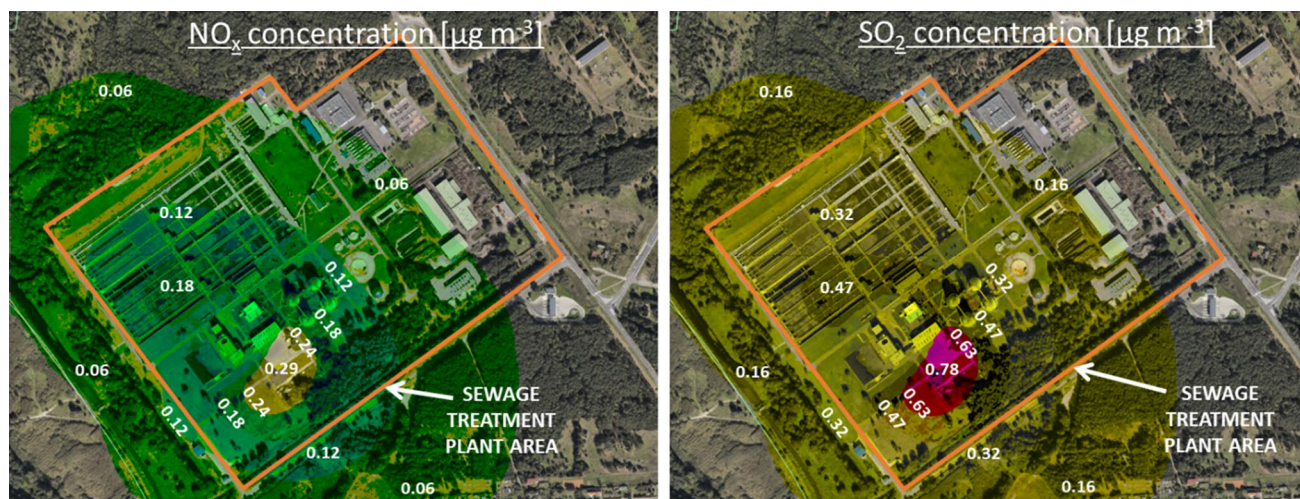


Fig. 4 Average annual concentration of NO_x and SO₂ emitted from the analyzed system

0.020 µg m⁻³ for PM₁₀ and 0.0070 µg m⁻³ for HCl (Figs. 4, 5). These values represent, respectively, 0.75, 4.00, 0.05,

and 0.07% of the acceptable average annual concentrations for these substances (as determined in Directive 2008/50/

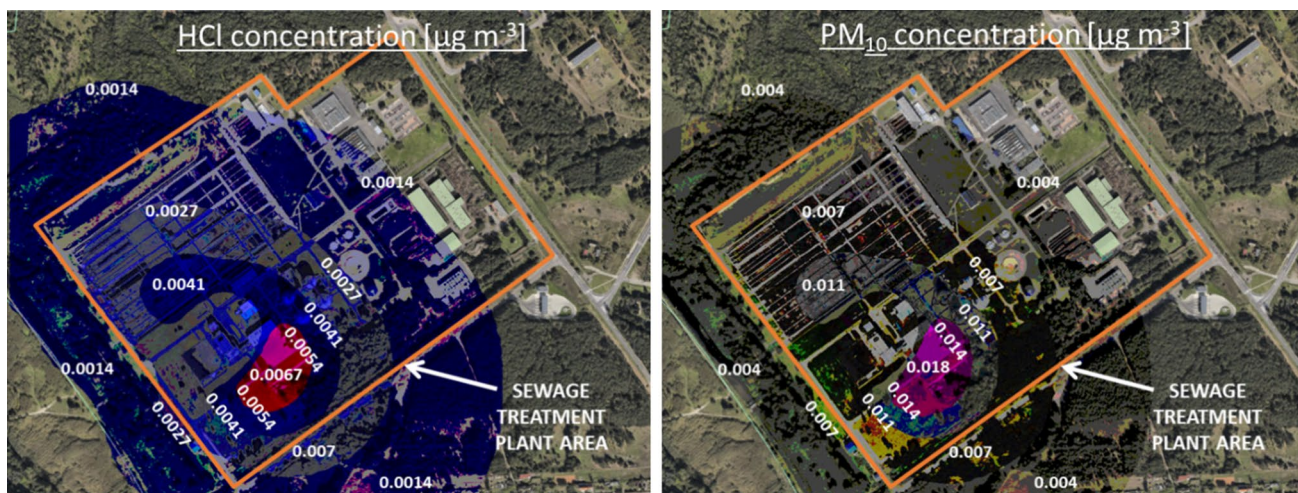


Fig. 5 Average annual concentration of HCl and PM₁₀ emitted from the analyzed system

EC). However, it should be remembered that the average hourly concentrations of pollution could be much higher in the case of maximum hourly emission.

To analyze the influence of physical parameters on the spread of emitted pollutants, flue gas conditions in the model were changed from real to nominal values. Calculations were made for a nominal temperature of 190 °C and nominal flue gas velocity of 14.16 m s⁻¹. The results of the numerical analysis with the nominal conditions did not differ significantly from those obtained with the real conditions. The highest annual concentration of air pollutants in the WWTP area decreased by only 0.02 μg m⁻³ for NO_x, by 0.05 μg m⁻³ for SO₂, by 0.002 μg m⁻³ for PM₁₀ and by 0.0005 μg m⁻³ for HCl. Thus, in the analyzed case there was no significant difference between the actual and the nominal conditions of exhaust gas flow.

Based on experimental measurements, the location of the TSTS had no significant impact on the concentration of air pollutants in the WWTP area. The “TSTS/background ratio” was calculated by dividing the concentration of air pollutants near the TSTS building by the concentration of “background” pollution (Fig. 6). The level of air pollutants (CO, CO₂, NO_x, SO₂, NH₃, CH₄, H₂S) in the vicinity of the TSTS was similar to the level of “background” pollution in the windward locations. These findings confirmed that only a low level of air pollution was caused by the TSTS, relative to the total concentration of pollutants in the air within the area of the WWTP. An exception was observed in the case of NH₃, the concentration of which was 2.0–3.5 times higher in the proximity of TSTS than in the remaining measurement points. This was due to the high concentrations of NH₃ near the TSTS in 2014, which were up to 8.6 times higher than the “background” concentration

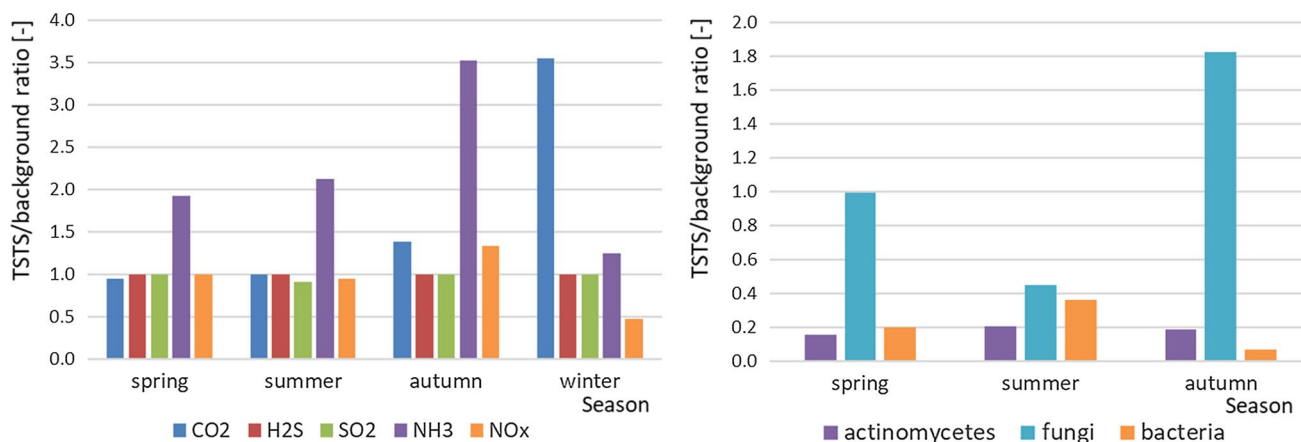


Fig. 6 Ratio of air pollutant concentration measured near the TSTS divided by the “background” pollution (“TSTS/background ratio”)

noted during measurements taken in November 2014. This finding is difficult to explain, especially given that the NH_3 emissions from the TSTS chimneys did not change significantly. Therefore, the increased concentration of NH_3 was probably caused by another technological unit of the WWTP, such as the composting facility.

Measurements performed during the winter revealed much higher concentrations of CO_2 than during other times of year, despite the fact that the operation of the system did not vary depending on the season. This increase may have had its origin in another WWTP technological units, such as the sludge chamber or composting plant (Fig. 1). The concentration of CH_4 varied depending on the date of measurement, and near the TSTS it ranged from 0.6 to 300 times the “background” value. However, the high CH_4 concentrations in the years 2013 and 2015 may be explained by the fact that part of the sewage sludge had been stored on a prism adjacent to the TSTS building.

The ratio of the concentration of biological agents measured near the TSTS divided by the “background” concentration was below 0.5 (with the exception of fungi). This suggests that neither the system associated with drying treated sludge nor the temporary storage of sludge posed a biological threat.

Additional measurements were made of biological and physical factors in April and June 2016. These measurements confirmed the limited impact of the analyzed TSTS on air quality. The total number of bacteria in the vicinity of the TSTS building did not exceed 1000 CFU/m^3 , and the total amounts of fungi amounted to 3300 CFU/m^3 . These values are higher than in other examined WWTP (Niazi et al. 2015). Within the TSTS building, the numbers were 1500 CFU/m^3 and 1200 CFU/m^3 , for bacteria and fungi, respectively. Physical factors inside the building and in its near vicinity, such as dusts and thermal energy, were also investigated. With one technological line working, the number of dust particles in 1 dm^3 of air ranged from about 23,000 to 135,000, while with two technological lines it ranged from about 55,000 to 276,000 (about twice as much as for one line). Thermal factors seemed to have a significant impact on the personnel operating the system. Thermal energy resulting from technological processes penetrated into the rooms of the building. The energy reached about 7.6% of the power of fluidized-bed furnaces (GOŚ–ŁAM corporate materials) and caused air temperatures in the tallest part of the building in excess of $37 \text{ }^\circ\text{C}$. These are unfavorable and potentially hazardous working conditions.

Although an important environmental consideration, the levels of heavy metals (Gerstle and Albrinck 2012) and dioxins (Wang et al. 2012) emitted from the TSTS were not investigated in our study. The scientific literature does not confirm that the emission of heavy metals and dioxins from

TSTS poses a health risk to either personnel (Carmen et al. 2003; Shih et al. 2006) or the local population.

Conclusions

It is essential to monitor the emission of pollution from thermal sludge treatment systems. Analyzing technological processes in terms of emissions enables swift action to be taken if the concentration of pollutants exceeds established limits (Wielgosiński et al. 2016). This study, carried out in the case of the Group Sewage Treatment Plant of Lodz (GOŚ ŁAM) in Poland, has considered the impact of thermal treatment of digested and dewatered sludge on air quality in the vicinity of a wastewater treatment plant. The operation of the thermal sludge treatment system was found to have a negligible influence on the concentrations of chemical and biological pollutants in the air. The concentrations of chemical substances associated with the operation of the thermal sludge treatment system did not exceed 1% of the maximum allowable average annual value (NO_x , PM_{10} , and HCl). This figure was slightly higher only in the case of SO_2 , which reached 4% of the maximum allowable average annual concentration. Experimental measurements revealed the concentrations of H_2S , SO_2 , and NO_x in the vicinity of the thermal sludge treatment system to be close to the “background” values. Much lower levels of bacteria and actinomycetes were observed than in other WWTP locations which have been studied. However, the concentrations of CO_2 , NH_3 , and CH_4 , as well as the number of colonies of fungi, were much higher than in the “background”, and varied depending on the measurement data. The variability of these values over time was possibly due to the influence of other technological units in the WWTP.

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