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Analysis of the Closures of Sub-grid Scale Variance of Reaction Progress Variable for Turbulent Bunsen Burner Flames at Different Pressure Levels

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Abstract

The statistical behaviour and modelling of the sub-grid variance of reaction progress variable have been analysed based on a priori analysis of direct numerical simulation (DNS) data of turbulent premixed Bunsen burner flames at different pressure levels. An algebraic expression for sub-grid variance, which can be derived based on a presumed bi-modal sub-grid distribution of reaction progress variable with impulses at unburned reactants and fully burned products, has been found to be inadequate for the purpose of prediction of sub-grid variance even for the flames in the wrinkled flamelets/corrugated flamelets regime. Moreover, an algebraic model, which is often used for modelling sub-grid variance of passive scalars, has been found to significantly overpredict the sub-grid variance of reaction progress variable for all the cases considered here. The modelling of the unclosed terms of the sub-grid variance transport equation has been analysed in detail. Suitable model expressions have been identified for the sub-grid flux of variance, reaction rate contribution and scalar dissipation rate based on a priori analysis of DNS data. It has been found that the alternation of pressure does not have any significant impact on the closures of sub-grid flux of variance but a model parameter for the Favre-filtered scalar dissipation rate needs to be modified to account for the variation of pressure.

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1 Introduction

In gas turbines and internal combustion engines, premixed turbulent combustion often takes place under elevated thermodynamic pressures. However, most combustion models have been proposed and validated at atmospheric conditions because of relative ease of conducting experiments and simulations for atmospheric pressure. The flame thickness decreases and turbulent Reynolds number increases (for a given set of values of root-mean-square velocity fluctuation and integral length scale) with increasing pressure and thus it often becomes challenging to analyse high-pressure premixed flames. The advances in high performance computing have enabled detailed analyses of high pressure premixed turbulent combustion and its associated modelling using direct numerical simulations (DNS) data (Savard et al. 2017; Klein et al. 2018a, b; Chakraborty et al. 2019; Alquallaf et al. 2019). The present paper focuses on the assessment of the closure of sub-grid scale (SGS) reaction progress variable variance under elevated pressure conditions for turbulent Bunsen burner flames. The SGS reaction progress variable variance σ_v^2 is defined as (Pierce and Moin 1998; Jimenez et al. 2001; Langella and Swaminathan 2016; Langella et al. 2016; Ranjan et al. 2016)

$$\sigma_v^2 = \widetilde{c^2} - \tilde{c}^2 \qquad (1)$$

where c is the reaction progress variable, and $\tilde{Q} = \overline{\rho Q}/\bar{\rho}$ and $\bar{Q}$ denote Favre-filtered and filtered value of a general variable Q, respectively with ρ being the gas density.

The closure of sub-grid scalar variance plays a crucial role in the modelling of micro-mixing in the context of Large Eddy Simulations (LES) (Pierce and Moin 1998; Jimenez et al. 2001). Moreover, σ_v^2 is a quantity of pivotal importance in turbulent premixed combustion modelling (Langella and Swaminathan 2016; Langella et al. 2016; Ranjan et al. 2016). The present analysis utilises an existing DNS database of turbulent Bunsen flames at different thermodynamic pressures representing the flamelet regime of combustion [flames with low Karlovitz number (i.e. $Ka < 1$)], which has been extended for this study by simulating a Bunsen flame with 25 times the baseline pressure. A recent study (Nilsson et al. 2019) focussed on the closure of the SGS variance σ_v^2 and its transport for high Karlovitz number flames but such an analysis is yet to be carried out for the low Karlovitz number conditions, located at the boundary of the wrinkled and the corrugated flamelets regimes, for a range of different thermodynamic pressures. This deficit in the existing literature has been addressed in the present work with a particular focus on the modelling of pressure effects on the unclosed terms in the transport equation of σ_v^2 for a range of different filter widths.

2 Mathematical Background and Numerical Implementation

An algebraic expression is often used for the evaluation of SGS variance of passive scalars in the following manner (Pierce and Moin 1998; Langella and Swaminathan 2016; Ranjan et al. 2016):

$$\sigma_v^2 = C\Delta^2 |\nabla \tilde{c}|^2 \qquad (2)$$

where $C = 0.5$ is the model constant (Ranjan et al. 2016) and Δ is the LES filter width. It is expected that σ_v^2 is affected by both chemical and turbulent processes (Chakraborty and Swaminathan 2011; Lai and Chakraborty 2016), which is not accounted for in Eq. 2. It is worth noting that σ_v^2 assumes the following expression:

$$\sigma_v^2 = \tilde{c}(1 - \tilde{c}) + O\big(Da_\Delta^{-1}\big) \tag{3}$$

subject to the assumption of a bimodal sub-grid probability density function (PDF) of c with impulses at $c = 0.0$ and $c = 1.0$. Here $Da_\Delta = \Delta S_L / u'_\Delta \delta_{th}$ is the sub-grid Damköhler number with $u'_\Delta = \sqrt{(\widetilde{u_i u_i} - \tilde{u}_i \tilde{u}_i)/3} = \sqrt{2k_{sgs}/3}$ and $k_{sgs} = (\widetilde{u_i u_i} - \tilde{u}_i \tilde{u}_i)/2$ being the SGS velocity fluctuation and the SGS turbulent kinetic energy, respectively. The term $O\big(Da_\Delta^{-1}\big)$ can be ignored only for $Da_\Delta \gg 1.0$, and under that condition, the maximum possible value of the SGS variance (i.e. $\sigma_v^2 = \tilde{c}(1 - \tilde{c})$) is obtained. However, the sub-grid PDF of c may not be bi-modal (Bray et al. 1985) and it might be necessary to solve a modelled transport equation of σ_v^2 in the cases where Eq. 2 and $\sigma_v^2 = \tilde{c}(1 - \tilde{c})$ do not provide satisfactory performance. The exact transport equation of σ_v^2 is given by:

$$\frac{\partial\big(\bar{\rho}\sigma_v^2\big)}{\partial t} + \frac{\partial\big(\bar{\rho}\tilde{u}_j\sigma_v^2\big)}{\partial x_j} = \underbrace{-\frac{\partial}{\partial x_j}\Big[\overline{\rho u_j c^2} - 2\big[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\big]\tilde{c} - \bar{\rho}\tilde{u}_j\widetilde{c^2}\Big]}_{T_1}$$

$$\underbrace{- 2\big[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\big]\frac{\partial \tilde{c}}{\partial x_j}}_{T_2} + \underbrace{2\big[\overline{\dot{w}c} - \overline{\dot{w}}\tilde{c}\big]}_{T_3} + \underbrace{\frac{\partial}{\partial x_j}\bigg(\rho D_c \frac{\partial \sigma_v^2}{\partial x_j}\bigg)}_{T_4} \underbrace{- 2\bar{\rho}\widetilde{\epsilon_c}}_{D_v} \tag{4}$$

where $u_j, \dot{w}$ and D_c are the jth component of velocity, reaction rate of progress variable and reaction progress variable diffusivity, respectively. In Eq. 4, $\widetilde{\epsilon_c} = \overline{\rho D_c \nabla c \cdot \nabla c}/\bar{\rho} - \widetilde{D_c}\nabla\tilde{c}\cdot\nabla\tilde{c}$ is the sub-grid scalar dissipation rate (SDR), whereas $\widetilde{N_c} = \overline{\rho D_c \nabla c \cdot \nabla c}/\bar{\rho}$ will henceforth be referred to as the Favre-filtered SDR in this paper. The term T_1 accounts for turbulent transport of SGS variance, whereas the term T_2 denotes generation/destruction of SGS variance due to $\nabla\tilde{c}$. The term T_3 accounts for generation/destruction of SGS variance due to chemical reaction rate, whereas T_4 depicts molecular diffusion of σ_v^2. The term $D_v = -2\bar{\rho}\widetilde{\epsilon_c}$ originates due to molecular dissipation of SGS variance under the action of SDR. In LES, the SGS flux of reaction progress variable $\big[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\big]$ is modelled in order to solve the transport equation of $\tilde{c}$, and thus the term T_2 can be considered to be closed. The modelling of $\big[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\big]$ has been discussed elsewhere (Gao et al. 2015a, b; Klein et al. 2016; 2018c) and thus is not repeated here. The molecular diffusion term T_4 is also a closed term and thus the closure of the transport equation of σ_v^2 depends on the modelling of T_1, T_3 and D_v. In the present analysis, the terms of Eq. 4 have been extracted to analyse their statistical behaviours by explicitly filtering the DNS data and T_1, T_3 and D_v extracted from DNS data have been utilised for assessment of their respective models.

For the purpose of this analysis, 6 different turbulent premixed Bunsen burner flames have been considered and these flames are taken from a database (which has been extended for this study) consisting of 16 different cases (Klein et al. 2018b). The chemical mechanism is simplified here using a single step irreversible reaction for the sake of computational economy so that a detailed parametric analysis involving different thermodynamic pressures can be conducted. The Reynolds number $Re = U_B d_n/\nu_u$ (based on the bulk inlet velocity U_B, nozzle diameter d_n, and the unburned-gas kinematic viscosity ν_u); turbulent Reynolds number $Re_t = u'l/\nu_u$; integral length scale to thermal flame thickness ratio l/δ_{th}; Damköhler number $Da = lS_L/\delta_{th}u'$; and Karlovitz number $Ka = (u'/S_L)^{3/2}(l/\delta_{th})^{-1/2}$ are listed in Table 1. Here $\delta_{th} = (T_{ad} - T_0)/\max|\nabla T|_L$ is the thermal flame thickness with

T_{ad} and T_0 being the adiabatic flame temperature and the unburned reactant temperature, respectively, and the subscript 'L' refers to the unstrained laminar flame quantities. The normalised mean inlet velocity is set to $U_B/S_L = 6.0$ and the normalised turbulent root-mean-square (rms) velocity fluctuation equals $u'/S_L = 1.0$, except for case D where u'/S_L at the inlet is 3.10. It is worth noting that there was a special reason for considering moderate turbulence intensities: due to an increasing ratio of the hydrodynamic to critical length scale, the flames become increasingly hydrodynamically unstable (e.g. Darrieus–Landau (DL) instability) with increasing pressure, which is an important point for modelling high pressure turbulent premixed flames. As the effects of DL instability are masked by turbulence effects for high turbulence intensities, a small value of normalised turbulent root-mean-square (rms) velocity fluctuation (u'/S_L) has been used in this work in order to be able to analyse the effects of DL instability at elevated pressure levels. The integral length scale to Bunsen burner nozzle diameter ratio is given by $l/d_n = 1/5$ except for case E where l/d_n is 3/5. For case F this corresponds to a ratio of $l/\delta_{th} = 25$ and in this sense the present database has much more realistic scale separation in terms of integral scale to thermal flame thickness (l/δ_{th}) than most existing DNS databases where l is of the same order as δ_{th}. The heat release parameter $\tau = (T_{ad} - T_0)/T_0$ and the Zel'dovich number $\beta = T_{ac}(T_{ad} - T_0)/T_{ad}^2$ are considered to be 4.5 and 6.0 respectively, and T_{ac} is the activation temperature. Standard values of Prandtl number ($Pr = 0.7$) and ratio of specific heats ($\gamma_g = 1.4$) have been used. All non-dimensional numbers in Table 1 are to be understood as the inlet values.

It can be noted from Table 1 that the turbulent Reynolds number Re_t increases from case A to case C to F. Furthermore, it can be seen from Table 1 that cases C, D and E have same values of Re_t but cases D and E have one tenth of the pressure of that of case C. The value of u'/S_L is higher in case D than in case C and E, whereas u'/S_L and l/δ_{th} values are exactly the same for cases C and E and thus they fall on the same point on the regime diagram (but behave very differently in terms of flame morphology). Although turbulent Reynolds number remains moderate for the cases considered here, it has been shown in the past that the model parameters for SDR reach an asymptotic value for $Re_t \approx 50.0$ (Chakraborty and Swaminathan 2013). Moreover, SDR models proposed using a priori analysis of moderate values of DNS data (Dunstan et al. 2013; Gao et al. 2014a) have been found to be perform well for flow configurations with much larger turbulent Reynolds number Re_t based on a posteriori analysis using LES (Ma et al. 2014a).

The simulations of high pressure Bunsen flames have been conducted by adjusting the viscosity and the Arrhenius parameters in such a way that $S_L \sim P^{-0.5}$, and $\nu_u \sim P^{-1}$ are satisfied, as that of methane-air flames (Turns 2011). Thus, the Zeldovich flame thickness δ_Z scales as $\delta_Z \sim P^{-0.5}$ (where $\delta_Z = \alpha_{T0}/S_L$ with α_{T0} being the thermal diffusivity in the unburned gas) and the numerical resolution must be adjusted accordingly. The

Table 1 The turbulence inlet flow parameters for the considered cases

Case	P/P_0	Re_D	Re_t	l/δ_{th}	Ka	Da
A	1	399	13.30	5.20	0.45	5.00
B	5	892	29.26	11.40	0.30	11.40
C	10	1262	41.22	16.13	0.25	16.13
D	1	399	41.22	5.20	2.40	1.670
E	1	399	41.22	16.13	0.25	16.13
F	25	1262	64.89	26.0	0.20	26.00

dimensions of the simulation domain are kept unchanged for all cases considered here and the nozzle diameter d_n corresponds roughly to half the domain size. Simulation domains of size $50\delta_{th} \times 50\delta_{th} \times 50\delta_{th}$ for $P = P_0$, $112\delta_{th} \times 112\delta_{th} \times 112\delta_{th}$ for $P = 5P_0$, $159\delta_{th} \times 159\delta_{th} \times 159\delta_{th}$ for $P = 10P_0$ and $250\delta_{th} \times 250\delta_{th} \times 250\delta_{th}$ for $P = 25P_0$ have been considered here, where P_0 is taken to be 1.0 bar (i.e. $P_0 = 1.0$ bar). Uniform Cartesian meshes of $250 \times 250 \times 250$, $560 \times 560 \times 560$, $795 \times 795 \times 795$ and $1272 \times 1272 \times 1272$ are used for cases A, D, E, case B, case C and case D, respectively, which ensure for all cases the resolution of the flame thickness and the smallest scales of turbulence (Klein et al. 2018a, b; Chakraborty et al. 2019; Alquallaf et al. 2019).

The simulations have been carried out using the DNS code SENGA (Jenkins and Cant 1999) in which the governing equations are solved using high order finite difference and Runge–Kutta time-advancement. Inflow data has been generated using a parallelised and modified version of the digital filter-based inflow methodology proposed by Klein et al. (2003) where the Gaussian filter in the temporal space has been replaced by an autoregressive AR1 process in order to avoid excessive filter length in this direction caused by the small-time step in the compressible flow solver. Interested readers are referred to Klein et al. (2018a) for further information regarding the DNS database considered here and its numerical implementation. The reacting scalar and flow fields have been initialised using an unstrained premixed laminar flame solution, which is specified as a function of radius from the nozzle centre. All the domain faces except for the inlet are specified using the partially non-reflecting NSCBC formalism (Poinsot and Lele 1992). The simulation time, when statistics were first taken, is chosen to be larger than two flow-through which corresponds to nearly four eddy-turnover times.

In this analysis, the DNS data has been explicitly LES filtered using a Gaussian filter kernel $G(r)$ so that the LES filtered values of a general quantity Q can be calculated as follows (Peters 2000; Nilsson et al. 2019; Chakraborty and Swaminathan 2011; Lai and Chakraborty 2016; Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a; Boger et al. 1998; Reddy and Abraham 2012; Chakraborty and Cant 2007, 2009):

$$\overline{Q(x)} = \int Q(x - r)G(r)dr, \quad G(r) = \left(6/\pi\Delta^2\right)^{3/2} \exp\left(-6r \cdot r/\Delta^2\right) \tag{5}$$

Results will be presented from $\Delta \approx 0.03d_n$ (corresponding for case A to the smallest filter width to flame thickness ratio of $\Delta/\delta_{th} = 0.8$) where the flame is partially resolved, up to $\Delta \approx 0.15d_n$ (corresponding for case F to the largest filter width to flame thickness ratio $\Delta/\delta_{th} = 19.0$) where the flame becomes fully unresolved and Δ becomes comparable to the integral length scale l.

3 Results and Discussion

The isosurfaces of $\tilde{c} = 0.5$ for cases A, C, E and F for $\Delta/d_n = 0.06$ and 0.15 are exemplarily shown in Fig. 1 along with instantaneous views of $c = 0.5$ isosurfaces of the corresponding cases. It can be seen from Fig. 1 that the flame morphology changes significantly with increasing pressure. The extent of wrinkling in cases C and F is significantly greater than in cases A and E due to DL instability (Klein et al. 2018a, b; Alquallaf et al. 2019) and interested readers are referred to Klein et al. (2018a, b) and Alquallaf et al. (2019) for further discussion on this aspect. Figure 1 further shows that the extent of wrinkling of the isosurface decreases with increasing Δ because of the smearing of local information due

Fig. 1 Isosurfaces of cases A, C, E and F for $\Delta/d_n = 0.06$ and 0.15 along with instantaneous views of $c = 0.5$
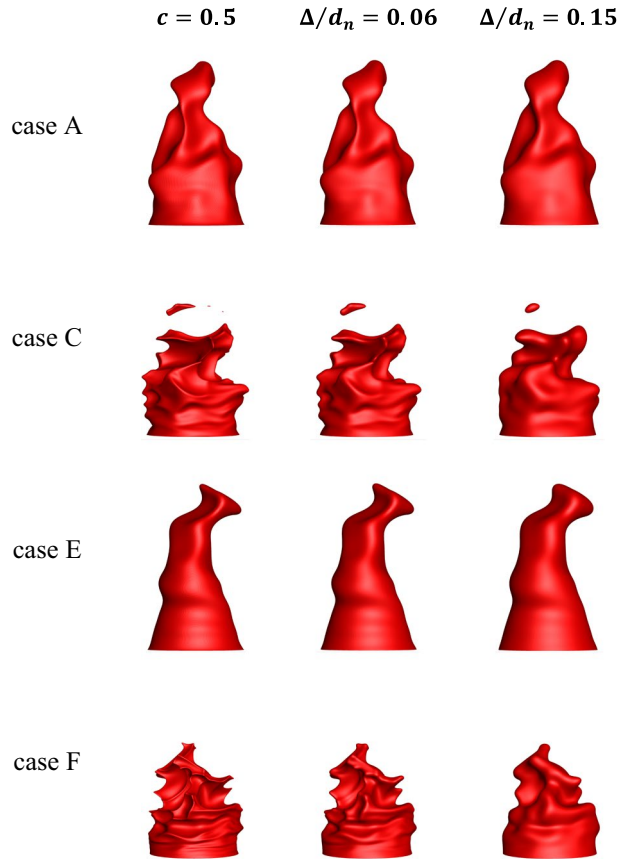

to the convolution operation associated with the filtering. For the sake of brevity, results will be shown for cases A, C and F only but results for cases B, D and E are qualitatively similar.

The variations of mean values of σ_v^2 conditional upon bins of $\tilde{c}$ for cases A, C, F for different values of Δ/d_n are shown in Fig. 2. It can be seen from Fig. 2 that σ_v^2 increases with increasing Δ before approaching an asymptotic value which is considerably smaller than the maximum possible value given by $\tilde{c}(1 - \tilde{c})$. The variation of mean values of Da_Δ conditional upon bins of $\tilde{c}$ for cases A, C, F for different normalised filter widths Δ/d_n is shown in Fig. 3, which shows that Da_Δ increases with increasing Δ but Da_Δ does not assume large (i.e. $Da_\Delta \gg 1$) values in all cases even for the largest value of Δ considered here. This is consistent with the analysis in Keil et al. (2019). Thus, the $O\left(Da_\Delta^{-1}\right)$ contribution can only be ignored for $Da_\Delta \gg 1$ and under that condition the maximum possible value of the SGS variance (i.e. $\sigma_v^2 = \tilde{c}(1 - \tilde{c})$) is obtained. Differences between σ_v^2 and $\tilde{c}(1 - \tilde{c})$ indicate the extent of the departure of the sub-grid PDF of c from the bi-modal distribution with impulses at $c = 0.0$ and 1.0, except for the largest filter width for case F which corresponds to $\Delta/\delta_{th} = 19$. This is consistent with previous findings (Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a; Chakraborty and Cant 2007, 2009).

In fact, Eq. 2 significantly overpredicts σ_v^2 and provides an unphysical prediction (i.e. $\sigma_v^2 > \tilde{c}(1 - \tilde{c})$) for all filter widths for the model parameter $C = 0.5$. Moreover, the ratio
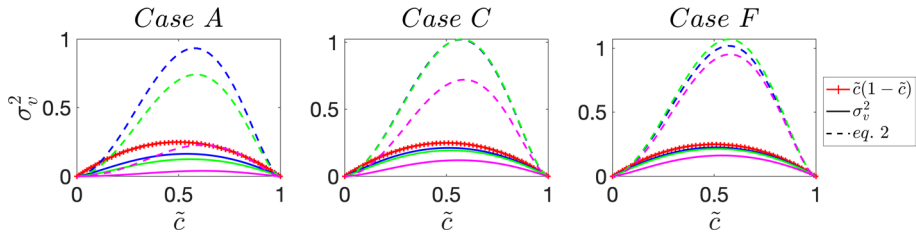
Fig. 2 Variations of mean values of σ_v^2 conditional upon bins of $\tilde{c}$ along with the predictions of Eq. 2 and $\tilde{c}(1 - \tilde{c})$ for $\Delta/d_n = 0.03$ (magenta), $\Delta/d_n = 0.09$ (green) and $\Delta/d_n = 0.15$ (blue) in cases A, C, F
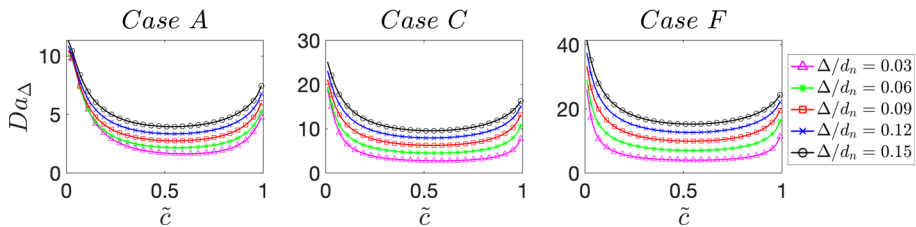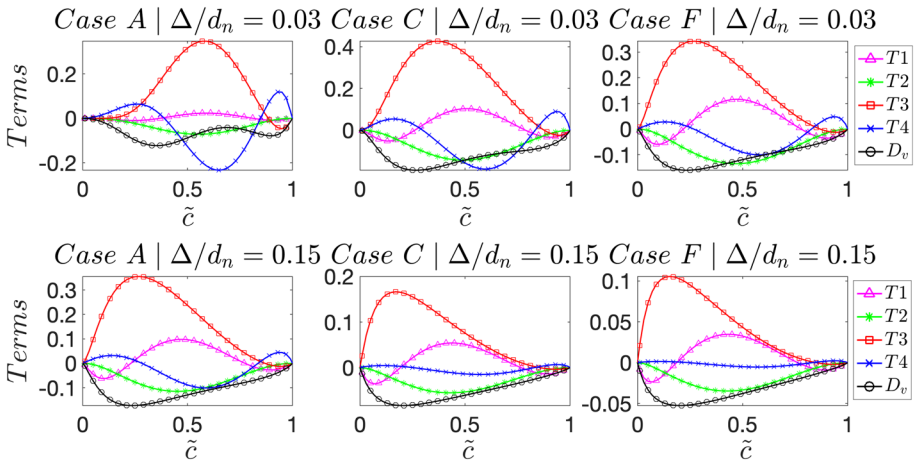

Fig. 3 Variations of mean values of Da_Δ conditional upon bins of $\tilde{c}$ for different Δ/d_n in cases A, C, F

$\sigma_v^2/\Delta^2|\nabla\tilde{c}|^2$ has been found to increase with increasing Δ and these values are different for each of the cases considered here (not shown). Thus, an alteration of C from 0.5 to a different value will not be sufficient for algebraic closure of σ_v^2 for all cases because the optimum value of C will not be a priori known.

The variations of $\{T_1, T_2, T_3, T_4 \text{ and } D_v\} \times \delta_{th}/\rho_0 S_L$ (with ρ_0 being the unburned gas density) conditional upon bins of $\tilde{c}$ for $\Delta/d_n = 0.03$ and 0.15 are shown in Fig. 4 for cases A, C, F. It can be seen from Fig. 4 that D_v acts as a leading order sink term for all cases irrespective of the filter width. By contrast, the reaction rate contribution T_3 acts as a leading order source term apart from the negative contribution towards the burned gas side of the flame brush for all cases for all filter widths considered here. For small values of Δ, $\widetilde{\epsilon_c} = \overline{\rho D_c \nabla c \cdot \nabla c}/\bar{\rho} - \tilde{D}\nabla\tilde{c} \cdot \nabla\tilde{c}$ tends to disappear as both $\overline{\rho D_c \nabla c \cdot \nabla c}/\bar{\rho}$ and $\tilde{D}_c\nabla\tilde{c} \cdot \nabla\tilde{c}$ approach $D_c\nabla c \cdot \nabla c$ (i.e. $lim_{\Delta\to 0}\overline{\rho D_c \nabla c \cdot \nabla c}/\bar{\rho} = D_c\nabla c \cdot \nabla c$ and $lim_{\Delta\to 0}\tilde{D}_c\nabla\tilde{c} \cdot \nabla\tilde{c} = D_c\nabla c \cdot \nabla c$) and as a result of this the magnitude of the mean contribution of D_v remains small for small filter widths but the relative magnitude of D_v in comparison to T_3 increases with increasing Δ as the sub-grid SDR $\widetilde{\epsilon_c}$ increases with an increase in filter width.

The mean contribution of the resolved scalar gradient term T_2 remains negative for all cases for all filter widths which is indicative of counter-gradient transport (i.e. $\left[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\right]\partial\tilde{c}/\partial x_j > 0$). The cases considered here are subjected to weak turbulence and thus the value of Bray number $N_B = \tau S_L/u'$ remains greater than unity (i.e. $N_B > 1.0$) for all cases. This suggests that the effects of flame normal acceleration dominate over those of turbulent velocity fluctuations leading to a dominant counter-gradient transport (Veynante et al. 1997). The magnitude of the mean contribution of T_2 remains smaller than that of T_3 for all cases considered here. The mean contribution of the molecular diffusion term T_4 remains positive on both unburned and burned gas sides of the flame brush with a negative dip in the middle of the flame brush in all cases irrespective of Δ, whereas the qualitative behaviour of

Fig. 4 Variations of mean values of $\{T_1, T_2, T_3, T_4 \text{ and } D_v\} \times \delta_{th}/\rho_0 S_L$ conditional upon bins of $\tilde{c}$ for $\Delta/d_n = 0.03$ and 0.15 in cases A, C, F

the mean values of the turbulent transport term T_1 remains just the opposite to that of T_4. This behaviour originates due to counter-gradient behaviour of the SGS flux of scalar variance, which will be discussed later in this paper. The magnitudes of mean contributions of T_4 in comparison to the magnitudes of D_v decrease with increasing Δ for all cases. It can further be seen from Fig. 4 that T_3 and D_v remain of the similar order of magnitude for large Δ (e.g. $\Delta/d_n = 0.15$ where $\Delta \gg \delta_{th}$) but this equilibrium is not maintained for small filter sizes (e.g. $\Delta/d_n = 0.03$ where $\Delta \leq \delta_{th}$).

The observed mean behaviours of T_1, T_2, T_3, T_4 and D_v have been found to be consistent with scaling estimates presented in Nilsson et al. (2019) and thus are not presented here. Moreover, the qualitative behaviours of the mean behaviours of T_1, T_2, T_3, T_4 and D_v have been qualitatively similar to those previously reported for high Karlovitz number detailed chemistry DNS (Nilsson et al. 2019) and simple chemistry DNS (Keil et al. 2019) data for the flames representing the thin reaction zones regime combustion. The mean behaviors of $\{T_1, T_2, T_3, T_4$ and $D_v\} \times \delta_{th}/\rho_0 S_L$ conditional upon bins of $\tilde{c}$ for $\Delta/\delta_{th} = 0.8$ and 4.0 in cases A, C, F are shown in the "Appendix". It becomes obvious that the behavior of the terms in the transport equation of σ_v^2 is very similar for different pressures when the same filter width to thermal flame thickness ratio is chosen. However, for a real LES simulation that will mean that the computational time increases drastically because the mesh size has to follow the decreasing flame thickness with increasing pressure.

Equation 4 indicates that the closure of T_1 depends on the appropriate closure of the SGS flux of variance $F_j = \left[\overline{\rho u_j c^2} - 2\left[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\right]\tilde{c} - \bar{\rho}\tilde{u}_j\tilde{c}^2\right]$. According to the gradient hypothesis model (GHM) (Langella and Swaminathan 2016; Langella et al. 2016) one gets:

$$F_j = \left[\overline{\rho u_j c^2} - 2\left[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c}\right]\tilde{c} - \bar{\rho}\tilde{u}_j\tilde{c}^2\right] = -\bar{\rho} Sc_t^{-1}(C_s\Delta)^2\sqrt{2\tilde{S}_{ij}\tilde{S}_{ij}}\,\partial\sigma_v^2/\partial x_j \tag{6}$$

where $C_s = 0.18$ is the Smagorinsky constant, $\tilde{S}_{ij} = 0.5\left(\partial\tilde{u}_i/\partial x_j + \partial\tilde{u}_j/\partial x_i\right)$ is the resolved strain rate and Sc_t is the turbulent Schmidt number. The mean values of $F_n/\rho_0 S_L$ (where F_n is the projection of the Flux F_j in resolved flame normal direction $-\nabla\tilde{c}/|\nabla\tilde{c}|$) conditional
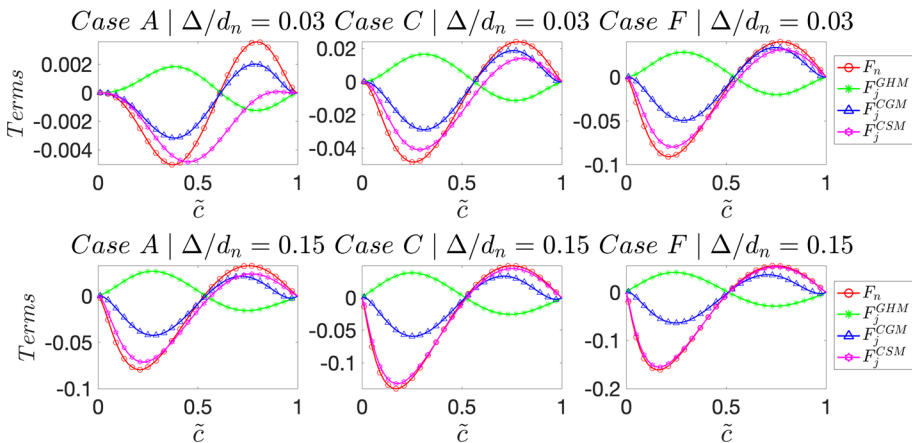
upon bins of $\tilde{c}$ are shown along with the prediction of F_j^{GHM} (for $Sc_t = 1.0$) in Fig. 5 for cases A, C, F for $\Delta/d_n = 0.03$ and 0.15. Figure 5 shows that F_j^{GHM} does not capture the qualitative behaviour of F_n and it predicts the opposite sign to the value obtained from DNS, which is indicative of the counter-gradient behaviour of the SGS variance flux. These findings are expected for these flames because the effects of flame normal acceleration are likely to overcome the influences of turbulent fluctuation to yield counter-gradient transport for small values of u'/S_L (Gao et al. 2015a, b; Klein et al. 2016, 2018c; Veynante et al. 1997). This suggests that it will be desirable to have a model which is capable of predicting both gradient and counter-gradient behaviours of F_j. It has been found in previous analyses that Clark's gradient model (CGM) (Clark et al. 1979) for SGS scalar flux (Gao et al. 2015a, b; Klein et al. 2016, 2018c) provides satisfactory performance, which has been utilised here to propose an alternative model as:

$$F_j = \left[\overline{\rho u_j c^2} - 2\left[\overline{\rho u_j c} - \bar{\rho}\tilde{u}_j\tilde{c} \right]\tilde{c} - \bar{\rho}\tilde{u}_j\tilde{c}^2 \right] = \bar{\rho}\frac{\Delta^2}{12}\frac{\partial\tilde{u}_j}{\partial x_k}\frac{\partial\sigma_v^2}{\partial x_k} \tag{7}$$

The predictions of F_j^{CGM} are also shown in Fig. 5 which indicates that this model is capable of capturing both gradient and counter-gradient behaviours of SGS flux of variance. However, the quantitative agreement between DNS data and model prediction deteriorates with increasing Δ.

A model expression, which was originally proposed by Chakraborty and Swaminathan (CSM) (2011) for the Reynolds flux of variance in the context of RANS, has been extended for LES in the present work in the following manner. According to Bray Moss Libby modelling (Bray et al. 1985) the Reynolds flux of variance can be expressed based on the presumed bi-modal PDF of c with impulses at $c = 0$ and $c = 1.0$ as:

$$\langle \rho u_i'' c''^2 \rangle = \langle \rho \rangle \widehat{c}\left(1 - \widehat{c}\right)[\langle u_i \rangle_P - \langle u_i \rangle_R](1 - 2\widehat{c}) + O(Da^{-1})$$

$$= \langle \rho u_i'' c'' \rangle (1 - 2\widehat{c}) + O(Da^{-1}) \tag{8}$$

Fig. 5 Variations of mean values of $F_n/\rho_0 S_L$ conditional upon bins of $\tilde{c}$ for $\Delta/d_n = 0.03$ and 0.15 in cases A, C, F along with the predictions of F_j^{GHM} (for $Sc_t = 1.0$), F_j^{CGM} and F_j^{CSM}

where $\langle q \rangle$ and $\hat{q} = \langle \rho q \rangle / \langle \rho \rangle$ are the Reynolds averaged and Favre-averaged values of a general quantity q, respectively and $\langle q \rangle_P$ and $\langle q \rangle_R$ are conditional mean values of the quantity q in products and reactants, respectively. However, Eq. 8 does not perform well for $Da < 1$ where the PDF of c does not remain bi-modal (Bray et al. 1985). The departure from bi-modal PDF can be quantified with the help of a segregation factor $g = \langle \rho c'' c'' \rangle / [\langle \rho \rangle \hat{c} (1 - \hat{c})]$ so that g increasingly deviates from unity with decreasing Damköhler number Da. In order to extend Eq. 8 for $Da < 1$ combustion, Chakraborty and Swaminathan (2011) proposed the following model expression and validated it with the help of a priori analysis:

$$\langle \rho u_i'' c''^2 \rangle = \langle \rho u_i'' c'' \rangle \left(1 - 2 \hat{c} \, g^m \right) [2g / (g + 1)] \; ; \; m = 0.3 \tag{9}$$
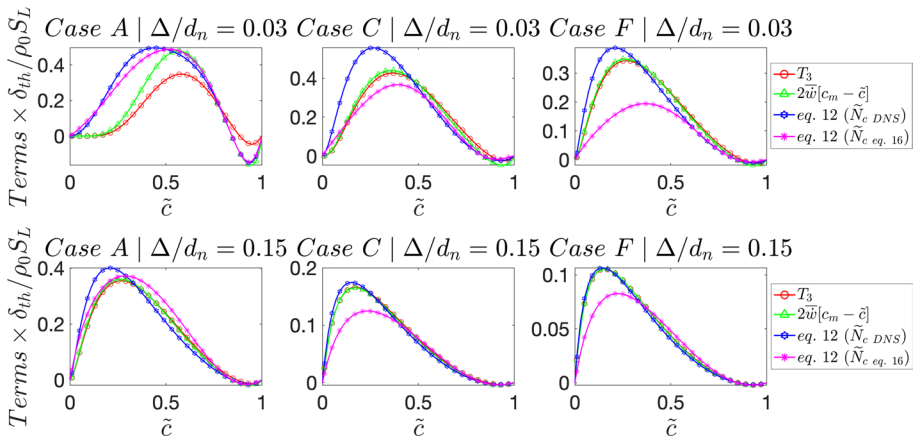
It can be seen from Eq. 9 that this expression reduces to Eq. 8 when $g = 1.0$ which is likely to be realised for $Da \gg 1$ where the PDF of c is likely to be bi-modal. In the context of LES, the model can be written as:

$$F_j^{CSM} = \left[\overline{\rho u_j c} - \bar{\rho} \tilde{u}_j \tilde{c} \right] \left[1 - 2\tilde{c} \left\{ \sigma_v^2 / \tilde{c}(1 - \tilde{c}) \right\}^{0.3} \right] \left\{ 2\sigma_v^2 / [\sigma_v^2 + \tilde{c}(1 - \tilde{c})] \right\} \tag{10}$$

Figure 5 shows that both qualitative and quantitative predictions of F_n can be obtained by using F_j^{CSM} for all filter widths and cases considered here. The satisfactory performance of F_j^{CSM} depends on appropriate modelling of the SGS scalar flux $\left[\overline{\rho u_j c} - \bar{\rho} \tilde{u}_j \tilde{c} \right]$, which has been addressed elsewhere (Gao et al. 2015a, b; Klein et al. 2016, 2018c) and thus is not repeated here.

The modelling of $T_3 = 2 \left[\overline{\dot{w} c} - \bar{\dot{w}} \tilde{c} \right]$ needs closures of $\bar{\dot{w}}$ and $\overline{\dot{w} c}$. For unity Lewis number flames, it is possible to write: $\bar{\dot{w}} = \int_0^1 [\dot{w}]_L P_\Delta(c) dc$ and $\overline{\dot{w} c} = \int_0^1 [\dot{w} c]_L P_\Delta(c) dc$ (Bray 1980) where $[q]_L$ is the value of a general variable q obtained from a flamelet table and $P_\Delta(c)$ is the presumed sub-grid PDF of c, which is usually parameterised using $\tilde{c}$ and σ_v^2 (Langella and Swaminathan 2016; Langella et al. 2016). Alternatively, it is possible to write: $\overline{\dot{w} c} = \bar{\dot{w}} c_m$ where $c_m = \int_0^1 [\dot{w} c]_L f(c) dc / \int_0^1 [\dot{w}]_L f(c) dc$ (Bray 1980), with $f(c)$ being the burning mode PDF, which can be taken as any appropriate continuous function according to Bray (Bray 1980). This thermo-chemical parameter c_m has been found to be 0.84 for cases A–F. Accordingly, T_3 can be expressed as: $T_3 = 2\bar{\dot{w}} \left[c_m - \tilde{c} \right]$. The variations of mean values of T_3 conditional upon bins of $\tilde{c}$ in cases A, C, F are shown in Fig. 6 for $\Delta / d_n = 0.03$ and 0.15, which shows that $2\bar{\dot{w}} \left[c_m - \tilde{c} \right]$ (with $\bar{\dot{w}}$ extracted from DNS data) satisfactorily captures both qualitative and quantitative behaviours of T_3 for all Δ in all cases considered here. According to Bray (Bray 1980), the mean reaction rate in the context of RANS for $Da \gg 1$ can be modelled by: $\langle \dot{w} \rangle = 2 \langle \rho N_c \rangle / (2c_m - 1)$. It has been shown in Dunstan et al. (2013), Gao et al. (2014a) and Ma et al. (2014a) based on a priori analysis of DNS that the expression $\bar{\dot{w}} = \{ 2\bar{\rho} \tilde{N}_c / (2c_m - 1) \}$ performs well for $\Delta / \delta_{th} \gg 1$ and the agreement between $\bar{\dot{w}}$ and $\{ 2\bar{\rho} \tilde{N}_c / (2c_m - 1) \}$ improves with increasing Δ, as sub-grid Damköhler number $Da_\Delta = \Delta S_L / u_\Delta' \delta_{th}$ increases with an increase in LES filter width (see Fig. 3). However, $\{ 2\bar{\rho} \tilde{N}_c / (2c_m - 1) \}$ does not adequately predict $\bar{\dot{w}}$ for small filter widths (i.e. $\Delta / \delta_{th} < 1$) when Da_Δ assumes small values. In order to obtain a single expression which predicts $\bar{\dot{w}}$ accurately for both small and large filter widths the following model expression was suggested in Dunstan et al. (2013), Gao et al. (2014a) and Ma et al. (2014a):

$$\bar{\dot{w}} = \{ 2\bar{\rho} \tilde{N}_c / (2c_m - 1) \} \times \{ 1 - \exp(-\phi \Delta / \delta_{th}) \} + f_1(\bar{\rho}, \tilde{c}, \tilde{T}) \exp(-\phi \Delta / \delta_{th}) \tag{11}$$

Fig. 6 Variations of mean values of $T_3 \times \delta_{th}/\rho_0 S_L$, $2\bar{\dot{w}}[c_m - \tilde{c}] \times \delta_{th}/\rho_0 S_L$ and the predictions of Eq. 12 (for $\tilde{N}_c$ extracted from DNS data and according to the prediction of Eq. 16 with β_c according to Eq. 18) conditional upon bins of $\tilde{c}$ for $\Delta/d_n = 0.03$ and 0.15 in cases A, C, F

where $f_1(\bar{\rho}, \tilde{c}, \tilde{T})$ is a function such that $\dot{w} = f_1(\rho, c, T)$ where T is the temperature, and $\phi = 0.56\delta_{th}S_L/\alpha_{T0}$ is a model parameter with α_{T0} being the thermal diffusivity in the unburned gas. The exponential terms $\exp(-\phi\Delta/\delta_{th})$ and $\{1 - \exp(-\phi\Delta/\delta_{th})\}$ act as bridging function such that one obtains $\bar{\dot{w}} = \{2\bar{\rho}\tilde{N}_c/(2c_m - 1)\}$ for $\Delta/\delta_{th} \gg 1$, and for $\Delta \to 0$, Eq. 11 reduces to $\lim_{\Delta \to 0}\bar{\dot{w}} = \dot{w} = \lim_{\Delta \to 0}f_1(\bar{\rho}, \tilde{c}, \tilde{T}) = f_1(\rho, c, T)$. It has been shown elsewhere (Gao et al. 2014a; Ma et al. 2014a) that the prediction of Eq. 11 shows better agreement with $\bar{\dot{w}}$ extracted from DNS data only for $\Delta > \delta_{th}$ and the quantitative agreement improves with increasing filter width. Using Eq. 11 in $T_3 = 2[\overline{\dot{w}c} - \bar{\dot{w}}\tilde{c}] = 2\bar{\dot{w}}\{c_m - \tilde{c}\}$ yields:

$$T_3 = 2[2\bar{\rho}\tilde{N}_c/(2c_m - 1)\{1 - \exp(-\phi\Delta/\delta_{th})\} + f_1(\bar{\rho}, \tilde{c}, \tilde{T})\exp(-\phi\Delta/\delta_{th})](c_m - \tilde{c}) \tag{12}$$

Figure 6 shows that T_3 can be reasonably predicted by this expression and the quantitative agreement improves with increasing Δ. This behaviour arises due to improved prediction of $\bar{\dot{w}}$ by Eq. 11 for large values of Δ (e.g. $\Delta = 0.15d_n$) (Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a).

The transport equation of $\tilde{N}_c$ takes the following form (Gao et al. 2014a, 2015c; Chakraborty et al. 2011):

$$\frac{\partial(\bar{\rho}\tilde{N}_c)}{\partial t} + \frac{\partial(\bar{\rho}\tilde{u}_j\tilde{N}_c)}{\partial x_j} = \underbrace{\overline{\frac{\partial}{\partial x_j}\left(\rho D\frac{\partial N_c}{\partial x_j}\right)}}_{D_1} + T_1' + T_2' + T_3' + T_4' - D_2 + f(D) \tag{13}$$

where u_j is the jth component of velocity vector and the terms on the left-hand side denote the transient effects and resolved advection of $\tilde{N}_c$ respectively. The term $D_1 = \overline{\nabla \cdot (\rho D\nabla N_c)}$ represents the molecular diffusion of $\tilde{N}_c$ and the terms $T_1', T_2', T_3', T_4', (-D_2)$ and $f(D)$ are unclosed and given by:

$$T_1' = -\frac{\partial}{\partial x_j}\left[\overline{\rho u_j N_c} - \bar{\rho}\tilde{u}_j \tilde{N}_c\right] \tag{14i}$$

$$T_2' = -\overline{\frac{2D}{\rho}\left[\dot{w} + \frac{\partial}{\partial x_j}\left(\rho D \frac{\partial c}{\partial x_j}\right)\right]\frac{\partial c}{\partial x_k}\frac{\partial \rho}{\partial x_k}} \tag{14ii}$$

$$T_3' = -2\overline{\rho D \frac{\partial c}{\partial x_i}\frac{\partial u_i}{\partial x_j}\frac{\partial c}{\partial x_j}} \tag{14iii}$$

$$T_4' = 2\overline{D\frac{\partial \dot{w}}{\partial x_i}\frac{\partial c}{\partial x_i}} \tag{14iv}$$

$$\left(-D_2\right) = -2\overline{\rho D^2 \frac{\partial^2 c}{\partial x_i \partial x_j}\frac{\partial^2 c}{\partial x_i \partial x_j}} \tag{14v}$$

$$f(D) = \overline{2D\frac{\partial c}{\partial x_k}\frac{\partial(\rho D)}{\partial x_k}\frac{\partial^2 c}{\partial x_j \partial x_j}} + \overline{2D\frac{\partial c}{\partial x_k}\frac{\partial^2(\rho D)}{\partial x_j \partial x_k}\frac{\partial c}{\partial x_j}} - \overline{\frac{\partial}{\partial x_j}\left(\rho N_c \frac{\partial D}{\partial x_j}\right)}$$
$$- \overline{2\rho D\frac{\partial D}{\partial x_j}\frac{\partial}{\partial x_j}\left(\frac{\partial c}{\partial x_k}\frac{\partial c}{\partial x_k}\right)} + \overline{\rho\left(\frac{\partial c}{\partial x_k}\frac{\partial c}{\partial x_k}\right)\left[\frac{\partial D}{\partial t} + u_j\frac{\partial D}{\partial x_j}\right]} \tag{14vi}$$

The term T_1' represents the effects of sub-grid convection, whereas T_2' denotes the effects of density-variation due to heat release. The term T_3' is determined by the alignment of ∇c with local strain rates $e_{ij} = 0.5\left(\partial u_i/\partial x_j + \partial u_j/\partial x_i\right)$ and this term is commonly referred to as the scalar-turbulence interaction term. The term T_4' arises due to the correlation between $\nabla \dot{w}$ and ∇c, whereas $\left(-D_2\right)$ denotes the molecular dissipation of scalar dissipation rate and these terms will henceforth be referred to as the reaction rate term and dissipation term respectively. The term $f(D)$ denotes the effects of D variation. It has been demonstrated based on scaling arguments by Gao et al. (2014b) that an equilibrium is maintained between the $\left(T_2' + T_3' + T_4' + f(D)\right)$ and $\left(-D_2\right)$ for large filter widths (i.e. $\Delta/\delta_{th} \gg 1$). A similar conclusion can be reached if the transport equation of $\widetilde{\varepsilon}_c = \langle\rho D\nabla c \cdot \nabla c\rangle/\langle\rho\rangle - \widetilde{D}\,\nabla\widehat{c}\cdot\nabla\widehat{c}$ is analysed and the terms equivalent to $\left(T_2' + T_3' + T_4' + f(D)\right)$ and $\left(-D_2\right)$ are considered (Chakraborty et al. 2008). Kolla et al. (2009) and Chakraborty and Swaminathan (2011) considered the modelled expressions for the terms equivalent to $T_2', T_3', \left(T_4' - D_2 + f(D)\right)$ in the context of RANS and utilised their balance (i.e. $\left(T_2' + T_3' + T_4' + f(D) - D_2\right) \approx 0$) to propose a model expression:

$$\widetilde{\varepsilon}_c = \left[2K_c^* S_L/\delta_{th} + (C_3^* - \tau Da_\Delta C_4^*)\widetilde{\varepsilon}/\widetilde{k}\right]\tilde{c}(1-\tilde{c})/\beta_c' \ ; \ \beta_c' = 6.7 \tag{15}$$

where C_3^*, C_4^* and β_c' are the model parameters and $K_c^* = (\delta_{th}/S_L)\int_0^1 \left[\rho N_c \nabla \cdot \vec{u}\right]_L f(c)dc/\int_0^1 \left[\rho N_c\right]_L f(c)dc$ is a thermo-chemical parameter (Chakraborty and Swaminathan 2011). Equation 15 has been extended to LES based on the equilibrium between the $\left(T_2' + T_3' + T_4' + f(D)\right)$ and $\left(-D_2\right)$ for large filter widths (i.e. $\Delta/\delta_{th} \gg 1$) in the following manner (Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a):

$$\tilde{N}_c = \tilde{D}\nabla\tilde{c}\cdot\nabla\tilde{c} + \left(1-f_b\right)\left[2K_c^*S_L/\delta_{th} + \left(C_3^* - \tau Da_\Delta C_4^*\right)2u_\Delta'/3\Delta\right]\tilde{c}(1-\tilde{c})/\beta_c \quad (16i)$$

The model parameters C_3^*, C_4^* and β_c are given by the following expressions (Gao et al. 2014a; Ma et al. 2014a):

$$C_3^* = \frac{2.0\sqrt{Ka_\Delta}}{1.0+\sqrt{Ka_\Delta}}; \quad C_4^* = \frac{1.2(1.0-\tilde{c})^{0.2}}{Le^{2.57}\left(1+Ka_\Delta\right)^{0.4}};$$

$$\beta_c = \max\left(\frac{2}{2c_m-1}, \left[1.05\frac{\tau}{\tau+1}+0.51\right]^{4.6}\right) \quad (16ii)$$

where $Ka_\Delta = \left(u_\Delta'/S_L\right)^{3/2}\left(\Delta/\delta_{th}\right)^{-1/2}$ is the sub-grid Karlovitz number. It is worth noting that β_c in LES is different from β_c' used in the context of RANS (Chakraborty and Swaminathan 2011; Kolla et al. 2009). The model parameter β_c (and β_c') originate from the model expression of $\left(T_4' - D_2 + f(D)\right)$. The combined contribution of the terms $D_1, T_4', \left(-D_2\right)$ and $f(D)$ can be written as (Chakraborty et al. 2008, 2011; Gao and Chakraborty 2016):

$$D_1 + T_4' - D_2 + f(D) \approx -2\overline{D\nabla\cdot\left(\rho S_d\vec{N}|\nabla c|\right)|\nabla c|} + 2\overline{\rho DS_d\nabla\cdot\vec{N}|\nabla c|^2} \quad (17)$$

where $S_d = [\dot{w} + \nabla\cdot(\rho D\nabla c)]/(\rho|\nabla c|)$ is the displacement speed. It can be seen with Eq. 17 that the net contribution of $\left[D_1 + T_4' - D_2 + f(D)\right]$ depends on flame curvature $\kappa_m = 0.5\nabla\cdot\vec{N}$ (with $\vec{N} = -\nabla c/|\nabla c|$ being the flame normal vector). This suggests that the model parameter β_c (and β_c') is likely to be dependent on flame curvature description in the underlying computational methodology. As flame wrinkling is partially resolved in LES in contrast to the total sub-grid curvature contribution in RANS, the modification from β_c' to β_c in the model expression of scalar dissipation rate is not completely unexpected. It is important to note that the model parameters C_3^*, C_4^* and β_c have been calibrated using a large number of DNS cases including variations of τ, Le, Da and Ka (see Gao et al. 2014a) in the past, and thus, the dependence of Ka is explicitly addressed.

In Eq. 16i (Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a), $K_c^* = (\delta_{th}/S_L)\int_0^1\left[\rho N_c\nabla\cdot\vec{u}\right]_Lf(c)dc/\int_0^1\left[\rho N_c\right]_Lf(c)dc$ is a thermo-chemical parameter (Chakraborty and Swaminathan 2011), which is found to be $K_c^* = 0.77\tau$ for cases A–F for the present thermo-chemistry and $f_b = \exp\left[-0.7\left(\Delta/\delta_{th}\right)^{1.7}\right]$ is a bridging function, that ensures that $\tilde{N}_c$ approaches $D\nabla c\cdot\nabla c$, when the flame is fully resolved (i.e. $\lim_{\Delta\to 0}\tilde{N}_c = D\nabla c\cdot\nabla c$). The model parameters C_3^*, C_4^* and β_c are given by Eq. 16ii (Gao et al. 2014a; Ma et al. 2014a), where $Ka_\Delta = \left(u_\Delta'/S_L\right)^{3/2}\left(\Delta/\delta_{th}\right)^{-1/2}$ is the sub-grid Karlovitz number. The predictions of Eq. 16i are compared to the mean values of $\tilde{N}_c$ extracted from DNS conditional upon the bins of $\tilde{c}$ in Fig. 7 for $\Delta/d_n = 0.03$ and 0.15, which shows that this model satisfactorily predicts $\tilde{N}_c$ for small filter widths (e.g. $\Delta/d_n = 0.03$) where the resolved component (i.e. $\tilde{D}\nabla\tilde{c}\cdot\nabla\tilde{c}$) plays the dominant role but over predictions can be observed for large filter widths (e.g. $\Delta/d_n = 0.15$). This is consistent with previous findings (Gao et al. 2014a; Ma et al. 2014a), which also showed that Eq. 16i overpredicts the mean values of $\tilde{N}_c$ conditional upon $\tilde{c}$ for small values of u'/S_L but this overprediction disappears for large values of u'/S_L. The extent of this overprediction is particularly severe for large filter widths (e.g. $\Delta/d_n = 0.15$) for high pressure cases B, C and F and the extent of overprediction increases with increasing pressure.

A given value of Δ/d_n implies larger value of Δ/δ_{th} for higher pressures as the flame thickness δ_{th} decreases with increasing pressure. The overprediction of the mean values of
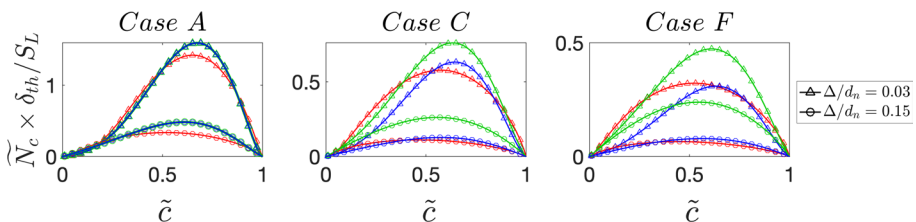
$\tilde{N}_c$ conditional upon $\tilde{c}$ according to Eq. 16i in cases B, C and F has been found to be comparable to that in cases A, D and E for a given value of Δ/δ_{th} (not shown here).

It has been shown elsewhere (Chakraborty and Swaminathan 2011; Chakraborty et al. 2008, 2011; Gao and Chakraborty 2016; Gao et al. 2016) that the model parameter β_c originates due to the curvature κ_m contribution to the SDR transport and κ_m dependence of S_d plays a key role in this contribution. It has been shown and discussed elsewhere (Klein et al. 2018b; Alquallaf et al. 2019) that the flame curvature statistics are significantly affected by pressure. The likelihood of obtaining DL instability increases with increasing pressure (Klein et al. 2018a, b; Alquallaf et al. 2019) and this is reflected in the increased skewness of negative curvature values in cases B, C and F (not shown here but refer to Klein et al. 2018a, b; Alquallaf et al. 2019). Thus, some pressure dependence of β_c is not unexpected. It has been found that the value of β_c, which ensures that the volume-integrated $\bar{\rho}\tilde{N}_c$ obtained from DNS data can be satisfactorily predicted, needs to increase with increasing pressure. This has been empirically parameterised as:

$$\beta_c = \max\left(2/(2c_m - 1), (p/p_0)^{0.37}\left[1.05\tau/(\tau + 1) + 0.51\right]^{4.6}\right) \tag{18}$$

It can be seen from Fig. 7 that the use of β_c expression given by Eq. 18 in Eq. 16 provides better agreement with DNS data. Furthermore, Fig. 7 shows that using Eq. 16i with β_c given by Eq. 18 in Eq. 12 provides satisfactory prediction of T_3 in all cases. It is worth noting that T_3 is overpredicted if Eq. 16i is used without the pressure dependence of β_c and thus is not explicitly shown here. Finally, as $\tilde{D}\nabla\tilde{c}\cdot\nabla\tilde{c}$ is a resolved quantity, Eq. 16i with β_c according to Eq. 18 can be used to close the molecular dissipation term $D_v = -\bar{\rho}\tilde{\varepsilon}_c = -\bar{\rho}[\tilde{N}_c - \tilde{D}\nabla\tilde{c}\cdot\nabla\tilde{c}]$.

In the present analysis all statistics are taken from the whole flame. This is based on the finding that there is little variation between different axial locations for a variety of quantities (Klein et al. 2018d). Finally, it is worth noting that the models discussed in this paper need to be implemented in actual LES simulations because numerical and modelling errors interact in a complex manner so the applicability of these models cannot entirely be assessed based on a priori DNS analysis. Interested authors are referred to (Vervisch et al. 2008) for discussion on the coupling between the numerical discretization of scalar field transport and the modelling of unresolved sub-grid scale fluctuations of chemical species. The novelty of the current analysis lies in the analysis of transport equation-based closure of SGS scalar variance for turbulent premixed flames under elevated pressures, which is yet to be carried out in the existing literature. Therefore, model capabilities are a priori assessed in this analysis without the interference

Fig. 7 Variations of mean values of $\tilde{N}_c \times \delta_{th}/S_L$ (red) and the predictions of Eq. 16i with β_c given by Eq. 16ii (green) and β_c according to Eq. 18 (blue) conditional upon bins of $\tilde{c}$ for $\Delta/d_n = 0.03$ and 0.15 in cases A, C, F

of numerical errors because a posteriori assessment of models using LES is intrinsically code dependent as a result of the interaction of numerical and modelling errors (Vervisch et al. 2008). It is worth noting that the same approach has been adopted in several previous studies (Ranjan et al. 2016; Nilsson et al. 2019; Reddy and Abraham 2012; Veynante et al. 1997; Charlette et al. 2002a; Selle and Bellan 2007; Lignell et al. 2009; Chatakonda et al. 2013; Lapointe and Blanquart 2017; Aspden et al. 2019; Devaud et al. 2019; Bushe et al. 2020) by other authors and there are several examples where the models proposed based on a priori DNS analysis (e.g. Gao et al. 2014a; Charlette et al. 2002a) have been demonstrated to perform well based on a posteriori assessment (e.g. Charlette et al. 2002b; Ma et al. 2013, 2014a, b; Butz et al. 2015). A recent analysis by different authors (Nilsson et al. 2019) on the modelling of SGS variance transport has also been conducted entirely by a priori assessment and the same approach has been adopted in the current study.

It is also worth mentioning that SGS variance transport has been adopted in several LES simulations (Langella and Swaminathan 2016; Langella et al. 2016, 2018; Massey et al. 2018; Chen et al. 2019a, b, 2020; Massey et al. 2019) in the past for atmospheric flames, and these simulations successfully used several model expressions considered in this analysis (e.g. Eqs. 6, 16i and 16ii) for closures of SGS flux of variance and SDR. The modelling of the chemical reaction contribution T_3 is reliant upon the SDR based filtered reaction rate closure given by Eq. 11. This SDR based reaction rate closure was also previously successfully implemented in LES albeit for atmospheric premixed turbulent combustion (Ma et al. 2014a; Butz et al. 2015) and the SDR closure given by Eqs. 16i and 16ii has been used in several previous LES studies (Ma et al. 2014a; Butz et al. 2015; Langella et al. 2018; Massey et al. 2018; Chen et al. 2019a, b, 2020; Massey et al. 2019) for atmospheric premixed combustion. The current analysis justifies the choices of the model expressions given by Eqs. 11, 16i and 16ii based on a priori DNS analysis. The only two expressions which are yet to be a posteriori analysed by implementing them in LES are the SGS variance flux model given by Eq. 10 and the pressure correction in the SDR modelling given by Eq. 18. A close inspection of Eq. 10 reveals that the success of this model depends on the successful modelling of SGS flux of reaction progress variable $\left[\overline{\rho u_j c} - \bar{\rho} \widetilde{u_j} \tilde{c} \right]$ and the modelling of $\left[\overline{\rho u_j c} - \bar{\rho} \widetilde{u_j} \tilde{c} \right]$ has been addressed elsewhere (Allauddin et al. 2017) by simultaneous a priori DNS and a posteriori LES analyses.

It is important to note that an experimental database, which offers information regarding SGS variance, and its sub-grid flux and dissipation rate for a range of elevated pressure conditions, is rare in the existing literature. Thus, a posteriori assessment of the models of the unclosed terms in the SGS variance transport equation is not a straightforward task because a discrepancy between LES results and experimental measurements may not originate from the inaccuracy in the SGS variance modelling and similarly a good agreement between LES and experimental results might be obtained due to fortuitous cancellation of errors. However, notwithstanding the above comments, the model expressions identified in this analysis need to be implemented in LES for an experimental configuration for which measurements are available for the assessment of the performances of the SGS variance closure.

4 Conclusions

The modelling of SGS variance of reaction progress variable and its sensitivity to thermodynamic pressure have been analysed based on a priori analysis of DNS data of turbulent premixed Bunsen burner flames at different pressure levels. An algebraic expression of the SGS variance based on the presumed bi-modal distribution with impulses at $c = 0.0$ and 1.0 has been found to be inadequate even for the flames in the corrugated/wrinkled flamelets regime. An alternative algebraic expression of SGS variance, which is usually used for passive scalar mixing, has been shown to significantly overpredict the corresponding quantity extracted from DNS data. The statistical behaviours of the unclosed terms of the SGS variance transport equation have been analysed. It has been found that the reaction rate contribution plays a leading order role for all filter widths and remains of the same order as that of the molecular dissipation contribution for large filter widths. The modelling of the unclosed terms of the SGS variance transport equation has been assessed based on a priori DNS analysis and suitable models have been identified for the SGS flux of variance, reaction rate contribution and scalar dissipation rate. One of the model parameters of a widely used algebraic closure of the Favre-filtered SDR closure (Dunstan et al. 2013; Gao et al. 2014a; Ma et al. 2014a) has been found to be dependent on pressure, whereas the model performance for the SGS flux of variance has been found to be independent of pressure variation. As the effects of Darrieus-Landau instability are likely to become weak for high values of Ka, the modelling methodology needs to be assessed for high pressure flames under high Karlovitz number. Moreover, these model expressions need to be implemented in actual LES for a posteriori assessment for comprehensive validation, which will form the basis of future analyses.
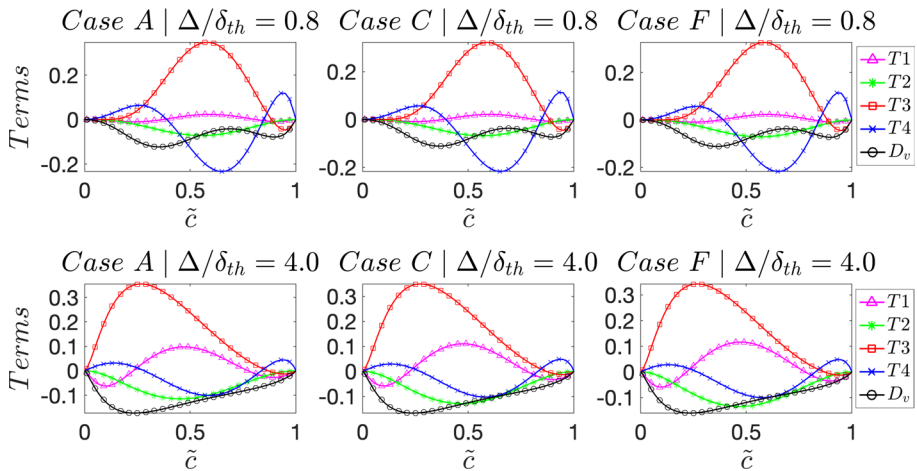
Compliance with Ethical Standards

Conflict of interest We have no competing interests.

Ethics Statement This work did not involve any active collection of human data.

Appendix

The mean behaviors of $\{T_1, T_2, T_3, T_4 \text{ and } D_v\} \times \delta_{th}/\rho_0 S_L$ conditional upon bins of $\tilde{c}$ for $\Delta/\delta_{th} = 0.8$ and 4.0 in cases A, C, F are shown in Fig. 8.

Fig. 8 Variations of mean values of $\{T_1, T_2, T_3, T_4 \text{ and } D_v\} \times \delta_{th}/\rho_0 S_L$ conditional upon bins of $\tilde{c}$ for $\Delta/\delta_{th} = 0.8$ and 4.0 for cases A, C, F

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