

Errata to: Coabsorbent and Thermal Recovery Compression Heat Pumping Technologies

Mihail-Dan Staicovici

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**M.-D. Staicovici, *Coabsorbent and Thermal Recovery Compression Heat Pumping Technologies*,
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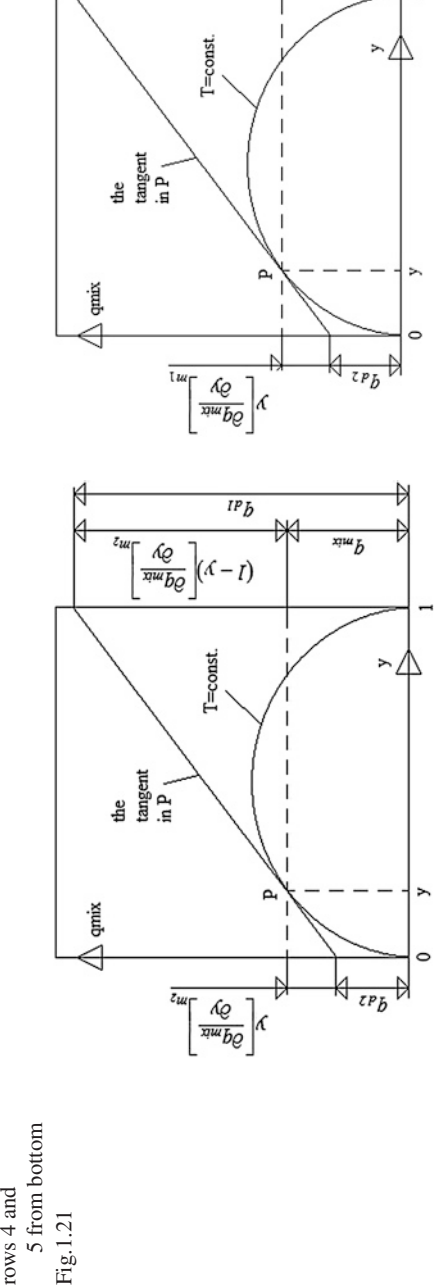
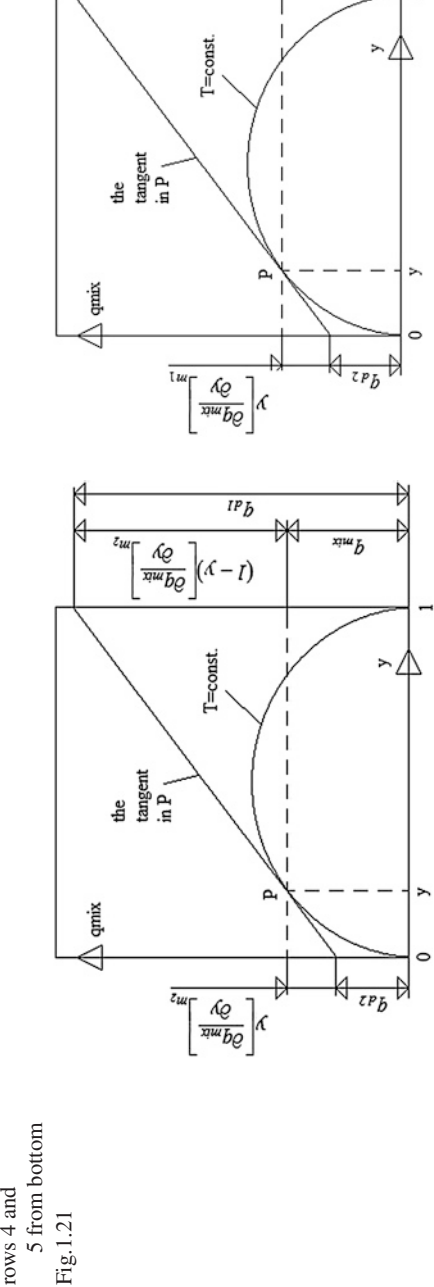
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Corrections to be made to the book "Coabsorbent and Thermal Recovery Compression Heat Pumping Technologies, author Mihail-Dan Staicovici

Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
viii, row 12 from top	The discharge gas superheat recovery is converted...	The recovered discharge gas superheat is converted...
17, row 14 from bottom	elaborated it 1824.	elaborated it in 1824.
21, row 10 from bottom	Than,	Then,
22, row 2 from bottom	in eqn. (1.98)	inequality (1.98)
22, row 5 from bottom	In in eqn. (1.98)	In inequality (1.98)
23, 1st row from top	In eqn. (1.100)	inequality (1.100)
23, row 8 from top	in eqn. (1.101)	inequality (1.101)
23, row 10 from top	In eqn. (1.102)	Inequality (1.102)
23, row 2 from bottom	in eqn. (1.108)	inequality (1.108)
23, row 3 from bottom	ineqn. (1.105)	Inequality (1.105)
23, row 12 from bottom	In in eqn. (1.105)	In inequality (1.105)
23, row 15 from bottom	In eqn. (1.103)	Inequality (1.103)
27, row 3 from top	calculated with the help the arithmetical mean	calculated with the help of the arithmetical mean

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Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
29, row 18 from bottom	where $-(dE)_{irrev}$ is the exergy dissipation	where $-\frac{\partial E}{\partial t}$ is the exergy dissipation
36, row 12 from bottom	free energy relationship as $U = F + TS$, Eq. (1.155),	free energy relationship as $U = F + TS$, Eq. (1.164),
45, row 7 from top	Eq. (1.208) partial derivatives are given by Eqs. (1.160) and (1.161) of Table 1.1, ...	Eq. (1.208) partial derivatives are given by Eqs. (1.169) and (1.170) of Table 1.1, ...
61, row 6 from top	Introducing Eq. (1.244) in Eq. (1.243), it is obtained:	Introducing Eqs. (1.244) and (1.243) in Eq. (1.242), it is obtained:
61, Eq. (1.248)	$\left[\frac{\partial q_{mix}}{\partial(1-y)} \right]_{m_1} \left[\frac{\partial(1-y)}{\partial m_2} \right]_{m_1} = -y \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_2}$	$\left[\frac{\partial q_{mix}}{\partial(1-y)} \right]_{m_1} \left[\frac{\partial(1-y)}{\partial m_2} \right]_{m_1} = -y \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_1}$
61, Eq. (1.249)	$q_{d2} = q_{mix} - y \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_2}$	$q_{d2} = q_{mix} - y \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_1}$
61, rows 4 and 5 from bottom	Eqs. (1.243) and (1.246)	Eqs. (1.242) and (1.249)
Fig.1.21		

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(Continued)	Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
62, Eq. (1.252)	62, rows 9 and 10 from bottom	$(1-y) \left[\frac{\partial q_{d1}}{\partial y} \right]_{m_2} + y \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_1} = 0$	$(1-y) \left[\frac{\partial q_{d1}}{\partial y} \right]_{m_1} + y \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_2} = 0$
62, rows 9 and 10 from bottom	62, rows 9 and 10 from bottom	Eqs. (1.245) and (1.249) of q_{d1} and q_{d2} are further partially derived with respect to y for $m_2 = \text{const.}$ and with respect to $(1-y)$ for $m_1 = \text{const.}$, respectively.	Eqs. (1.245) and (1.249) of q_{d1} and q_{d2} are further partially derived with respect to y for $m_1 = \text{const.}$ and with respect to $(1-y)$ for $m_2 = \text{const.}$, respectively.
62, Eq. (1.253)	62, Eq. (1.253)	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_2} + \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_1} = 0$	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_1} + \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_2} = 0$
62, Eq. (1.254)	62, Eq. (1.254)	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_2} - \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_1} = -2 \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_1} - \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_2}$	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_1} - \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_2} = 2 \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_1} - \left[\frac{\partial q_{mix}}{\partial y} \right]_{m_2}$
62, row 3 from bottom	62, row 3 from bottom	Equations (1.252) and (1.253) are solved together for $\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_2}$ and $\left[\frac{\partial q_{d2}}{\partial y} \right]_{m_1}$, obtaining:	Equations (1.252) and (1.253) are solved together for $\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_1}$ and $\left[\frac{\partial q_{d2}}{\partial y} \right]_{m_2}$, obtaining:
62, Eq. (1.255)	62, Eq. (1.255)	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_2} = \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_1} = 0$	$\left[\frac{\partial q_{d1}}{\partial y} \right]_{m_1} = \left[\frac{\partial q_{d2}}{\partial y} \right]_{m_2} = 0$
70, row 7 from bottom	70, row 7 from bottom	The specific Gibbs free enthalpy is at the same time the chemical potential of the system, $\varphi = \left(\frac{\partial \Phi}{\partial G} \right)_{T,p}$, according to eqn. (1.163).	The specific Gibbs free enthalpy is at the same time the chemical potential of the system, $\varphi = \left(\frac{\partial \Phi}{\partial G} \right)_{T,p}$ according to eqn. (1.172).
70, row 9 from bottom	70, row 9 from bottom	specific Gibbs free enthalpy assessment, $\varphi, \varphi = \frac{\Phi}{G}$, $(\Phi(T, p) = H - TS, \text{Table 1.1, eqn. (1.159)}) \dots$	specific Gibbs free enthalpy assessment, $\varphi, \varphi = \frac{\Phi}{G}$, $(\Phi(T, p) = H - TS, \text{Table 1.1, eqn. (1.168)}) \dots$
73, row 12 from bottom	73, row 12 from bottom	In eqn. (1.283), the last bracket of the right member can be calculated from eqns. (1.276) and (1.277)...	In eqn. (1.283), the last bracket of the right member can be calculated from gas phase eqns. (1.276) and (1.277)...
75, row 3 from bottom	75, row 3 from bottom	<i>Gas phase:</i> $c_p^d(T, p_0) = b_1 + b_2 T + b_3 T^2 \text{ (1.294)}$ $v^g(T, p) = \frac{RT}{p} + c_1 + \frac{c_2}{T^3} + \frac{c_3}{T^4} + \frac{c_4 p^2}{T^4} \text{ (1.295)}$	<i>Gas phase:</i> $c_p^d(T, p_0) = b_1 + b_2 T + b_3 T^2 \text{ (1.294)}$ $v^g(T, p) = \frac{RT}{p} + c_1 + \frac{c_2}{T^3} + \frac{c_3}{T^4} + \frac{c_4 p^2}{T^4} \text{ (1.295)}$

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Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
75,	$(Y = 0; Y = 0)$	$(Y = 0; Y = 1)$
row 5 from top		
78,	Introducing eqns. (1.295), (1.296) and (1.306) in eqn. (1.304), the analytical expression of the gas phase free enthalpy results:	Introducing eqns. (1.295), (1.296) and (1.306) in eqn. (1.307), the analytical expression of the gas phase free enthalpy results:
1st row from top		
128,	This time, temperature is the internal heating temperature....	This time, T_M temperature is the internal heating temperature....
row 8 from the bottom		
186,	for seen	foreseen
row 6 from top		
208,	Fig. 4.44	Fig. 4.45
Caption of Fig. 4.17		
208,	(see Fig. 4.44 of Sect. 4.3.2)	(see Fig. 4.45 of Sect. 4.3.1)
row 2 from top		
209,	Fig. 4.44	Fig. 4.43
row 2 from the top		
210,	$\gamma_{GO,1}$	$\Delta T_{gax,R}$
row 5 from bottom		
211,	$\Delta T_{R,i,gax}(\Delta T_{gax,R,max})$	$\gamma_{R,i,gax} = \gamma_{R,i,gax}(\Delta T_{gax,R,max})$
row 6 from top		
212,	$\Delta T_{gax,R,max} \leq \Delta T_{gax,R} \leq \Delta T_{gax,R,max}$	$\Delta T_{gax,R,min} \leq \Delta T_{gax,R} \leq \Delta T_{gax,R,max}$
row 3 from the bottom		
214,	$\gamma_{G,j,gax}^e$	$\gamma_{G,j,gax}^e$
4th row down from Eq. (4.122)		
215,	Fig. 4.37a of Sect. 4.2.3	Fig. 4.38a of Sect. 4.2.3
7th row down from Eq. (4.129)		
215,	GHE-Gax problem study cases	GHE-Gax problem study cases

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Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
215, row 3 from the bottom	Resorber Heat Excess (RHE) Gax Operation Model	Generator Heat Excess (GHE) Gax Operation Model
215, row 12 from the bottom	Results of the RHE-Gax Model Run with $\Delta T_{gax,r,\min}$ Infinite Equivalent Solutions to A GHE-Gax Problem	Results of the GHE-Gax Model Run with an intermediate $\Delta T_{gax,G}$ Infinite Equivalent Solutions to a GHE-Gax Problem
216, row 12 down from the top	$q_{G,1,gax}^e = 574.6$	$q_{G,1,gax}^e = 574.6$
218, row 5 from the bottom	According to the 6th study case, running the 4.2.1.3.2. sub-sub-paragraph model for the configuration...	According to the 6th study case, running the Sect. Generator Heat Excess (GHE) Gax Operation Model for the configuration...
250, row 13 from top	Equations (5.6) and (1.214)...	Equations (5.6) and (1.223)...
251, row 2 from bottom	Eq. (1.217)...	Eq. (1.226)...
265, row 3 from top	Important properties of the cascades at hand is emphasized next	Important properties of the cascades at hand are emphasized next
266, row 2 from top	Eq. (1.81)...	Eq. (1.65)...
266, row 6 from top	Eqs. (5.81) (5.82), (5.76) and (5.77)	Eqs. (5.81) and (5.82), Eqs. (5.76) and (5.77)
267, row 7 from top	Eqs. (1.208) and (1.209)...	Eqs. (1.217) and (1.218)...
267, row 6 from bottom	Eqs. (1.208) and (1.209)...	Eqs. (1.217) and (1.218)...

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(Continued)	Present text	Corrections to be made = the text which the "Present text" must be replaced with (last column, the CO ₂ -NH ₃ known cascade).
268,	(last column, the CO ₂ -NH ₃ known cascade). Table 5.3.	(last column, the CO ₂ -NH ₃ known cascade).
1st row from bottom	Appendix 1	Appendix 7
row 18 from bottom	, it results that in Eq. ...	, it results that inequality ...
309,	Indeed, from the obvious in equations	Indeed, from the obvious inequalities
row 12 from bottom	Appendix 2	Appendix 7
309,	Appendix 1	Appendix 7
row 13 from bottom	Equation (7.34) ...	i) Equation (7.34) ...
315,	Considering in Eqs. (A7.1, 7.20, 7.28) ...	Considering in Eq. (A7.1), Eqs. (7.19, 7.28) ...
1 st row from bottom	Appendix 2	ii) A simple, yet not simplistic, explanation ...
324,	Appendix 1	Appendix 8
row 7 from top	(see Appendix 1 of this chapter)	(see Appendix 8 of this chapter)
324,	Appendix 1	Appendix 8
row 13 from top	Appendix 1	Appendix 8
324,	Appendix 1	Appendix 8
row 14 from top	Appendix 1	Appendix 8
331,	Appendix 1	Appendix 8
row 12 from top	Appendix 1	Appendix 8
334,	Appendix 1	Appendix 8
row 2 from top	Appendix 1	Appendix 8
338,	Appendix 1	Appendix 8
row 13 from bottom	Appendix 1	Appendix 8
338,	Appendix 1	Appendix 8
row 16 from bottom	Appendix 1	Appendix 8

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(Continued)	Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
369,	Appendix 1		Appendix 8
1st row from bottom			
369,			
row 7 from bottom		$1 > \frac{n+1}{n+2}x < 1$	$\frac{n+1}{n+2}x < 1$
373,	Appendix 1		Appendix 8
row 4 from bottom			
375,			
1st row			$\eta_C(\xi) = 1 - \frac{\ln \frac{T_{2a}}{T_1}}{\frac{T_{2a}}{T_1} - 1} \equiv \eta_{C,IFC} = \quad (A8.4)$ $= 1 - \frac{2T_1}{T_{2a} - T_1} \frac{T_{2a} - T_1}{T_{2a} + T_1}$ $T_{ax} - T_{2a}$
378,	$T_{ax} - T_{2a}$		
row 4 from top			
391,	(see Appendix of this chapter)		(see Appendix 9 of this chapter)
row 6 from top			
403,	Eqs. (9.57) and (9.70)		Eqs. (9.56) and (9.70)
row 2 from top			
430,	(see Appendix)		(see Appendix 9)
row 2 from bottom			
431,	(see Appendix)		(see Appendix 9)
row 10 from top			
449,			
Eq. (9.180)	$\frac{h_1 - h_2}{T_{f,w}} + \frac{h_3 - h_4}{T_{f,s}} + (h_{ep,w,2} - h_{ep,w,1}) \left(\frac{1}{T_{f,w}} - \frac{1}{T_{ep,w}} \right)$ $+ (h_{f,s,4} - h_{f,s,3}) \left(\frac{1}{T_{f,s}} - \frac{1}{T_{ep,s}} \right)$	$\frac{h_1 - h_2}{T_{f,w}} + \frac{h_3 - h_4}{T_{f,s}} + (h_{ep,w,2} - h_{ep,w,1}) \left(\frac{1}{T_{f,w}} - \frac{1}{T_{ep,w}} \right)$ $+ (h_{f,s,4} - h_{f,s,3}) \left(\frac{1}{T_{f,s}} - \frac{1}{T_{ep,s}} \right) = 0$	

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Page	Present text	Corrections to be made = the text which the "Present text" must be replaced with
451,	Appendix 1	Appendix 9
row 12 from top	The natural ...	i) The natural ...
451,	Appendix 1	
row 13 from top	Using the vector ...	ii) Using the vector ...
452,	Appendix	Appendix 10
row 3 from top	Appendix	Appendix 10
452,	The Heat/sink sources...	The heat/sink sources...
row 3 from top		
463,		
row 2 from top		
465,		
row 14 from top		
495,		
row 3 from bottom		